

§ 63.9780

40 CFR Ch. I (7-1-17 Edition)

Subpart SSSSS—National Emission Standards for Hazardous Air Pollutants for Refractory Products Manufacturing

SOURCE: 68 FR 18747, Apr. 16, 2003, unless otherwise noted.

WHAT THIS SUBPART COVERS

§ 63.9780 What is the purpose of this subpart?

This subpart establishes national emission standards for hazardous air pollutants (NESIIAP) for refractory products manufacturing facilities. This subpart also establishes requirements to demonstrate initial and continuous compliance with the emission limitations.

§ 63.9782 Am I subject to this subpart?

You are subject to this subpart if you own or operate a refractory products manufacturing facility that is, is located at, or is part of, a major source of hazardous air pollutant (HAP) emissions according to the criteria in paragraphs (a) and (b) of this section.

(a) A refractory products manufacturing facility is a plant site that manufactures refractory products (refractory bricks, refractory shapes, monolithics, kiln furniture, crucibles, and other materials used for lining furnaces and other high temperature process units), as defined in § 63.9824. Refractory products manufacturing facilities typically process raw material by crushing, grinding, and screening; mixing the processed raw materials with binders and other additives; forming the refractory mix into shapes; and drying and firing the shapes.

(b) A major source of HAP is a plant site that emits or has the potential to emit any single HAP at a rate of 9.07 megagrams (10 tons) or more per year or any combination of HAP at a rate of 22.68 megagrams (25 tons) or more per year.

§ 63.9784 What parts of my plant does this subpart cover?

(a) This subpart applies to each new, reconstructed, or existing affected source at a refractory products manufacturing facility.

(b) The existing affected sources are shape dryers, curing ovens, and kilns that are used to manufacture refractory products that use organic HAP; shape preheaters, pitch working tanks, defumers, and coking ovens that are used to produce pitch-impregnated refractory products; kilns that are used to manufacture chromium refractory products; and kilns that are used to manufacture clay refractory products.

(c) The new or reconstructed affected sources are shape dryers, curing ovens, and kilns that are used to manufacture refractory products that use organic HAP; shape preheaters, pitch working tanks, defumers, and coking ovens used to produce pitch-impregnated refractory products; kilns that are used to manufacture chromium refractory products; and kilns that are used to manufacture clay refractory products.

(d) Shape dryers, curing ovens, kilns, coking ovens, defumers, shape preheaters, and pitch working tanks that are research and development (R&D) process units are not subject to the requirements of this subpart. (See definition of *research and development process unit* in § 63.9824).

(e) A source is a new affected source if you began construction of the affected source after June 20, 2002, and you met the applicability criteria at the time you began construction.

(f) An affected source is reconstructed if you meet the criteria as defined in § 63.2.

(g) An affected source is existing if it is not new or reconstructed.

§ 63.9786 When do I have to comply with this subpart?

(a) If you have a new or reconstructed affected source, you must comply with this subpart according to paragraphs (a)(1) and (2) of this section.

(1) If the initial startup of your affected source is before April 16, 2003, then you must comply with the emission limitations for new and reconstructed sources in this subpart no later than April 16, 2003.

(2) If the initial startup of your affected source is after April 16, 2003, then you must comply with the emission limitations for new and reconstructed sources in this subpart upon initial startup of your affected source.

(b) If you have an existing affected source, you must comply with the emission limitations for existing sources no later than April 17, 2006.

(c) You must be in compliance with this subpart when you conduct a performance test on an affected source.

(d) If you have an existing area source that increases its emissions or its potential to emit such that it becomes a major source of HAP, you must be in compliance with this subpart according to paragraphs (d)(1) and (2) of this section.

(1) Any portion of the existing facility that is a new affected source or a new reconstructed source must be in compliance with this subpart upon startup.

(2) All other parts of the existing facility must be in compliance with this subpart by 3 years after the date the area source becomes a major source.

(e) If you have a new area source (i.e., an area source for which construction or reconstruction was commenced after June 20, 2002) that increases its emissions or its potential to emit such that it becomes a major source of HAP, you must be in compliance with this subpart upon initial startup of your affected source as a major source.

(f) You must meet the notification requirements in § 63.9812 according to the schedule in § 63.9812 and in 40 CFR part 63, subpart A. Some of the notifications must be submitted before you are required to comply with the emission limitations in this subpart.

EMISSION LIMITATIONS AND WORK PRACTICE STANDARDS

§ 63.9788 What emission limits, operating limits, and work practice standards must I meet?

(a) You must meet each emission limit in Table 1 to this subpart that applies to you.

(b) You must meet each operating limit in Table 2 to this subpart that applies to you.

(c) You must meet each work practice standard in Table 3 to this subpart that applies to you.

§ 63.9790 What are my options for meeting the emission limits?

To meet the emission limits in Table 1 to this subpart, you must use one or

both of the options listed in paragraphs (a) and (b) of this section.

(a) *Emissions control system.* Use an emissions capture and collection system and an add-on air pollution control device (APCD) and demonstrate that the resulting emissions or emissions reductions meet the applicable emission limits in Table 1 to this subpart, and demonstrate that the capture and collection system and APCD meet the applicable operating limits in Table 2 to this subpart.

(b) *Process changes.* Use raw materials that have little or no potential to emit HAP during the refractory products manufacturing process or implement manufacturing process changes and demonstrate that the resulting emissions or emissions reductions meet the applicable emission limits in Table 1 to this subpart without an add-on APCD.

GENERAL COMPLIANCE REQUIREMENTS

§ 63.9792 What are my general requirements for complying with this subpart?

(a) You must be in compliance with the emission limitations (including operating limits and work practice standards) in this subpart at all times, except during periods specified in paragraphs (a)(1) and (2) of this section.

(1) Periods of startup, shutdown, and malfunction.

(2) Periods of scheduled maintenance on a control device that is used on an affected continuous kiln, as specified in paragraph (e) of this section.

(b) Except as specified in paragraph (e) of this section, you must always operate and maintain your affected source, including air pollution control and monitoring equipment, according to the provisions in § 63.6(e)(1)(i). During the period between the compliance date specified for your affected source in § 63.9786 and the date upon which continuous monitoring systems have been installed and validated and any applicable operating limits have been established, you must maintain a log detailing the operation and maintenance of the process and emissions control equipment.

(c) You must develop a written startup, shutdown, and malfunction plan (SSMP) according to the provisions in § 63.6(e)(3).

(d) You must prepare and implement a written operation, maintenance, and monitoring (OM&M) plan according to the requirements in § 63.9794.

(e) If you own or operate an affected continuous kiln and must perform scheduled maintenance on the control device for that kiln, you may bypass the kiln control device and continue operating the kiln upon approval by the Administrator, provided you satisfy the conditions listed in paragraphs (e)(1) through (3) of this section.

(1) You must request approval from the Administrator to bypass the control device while the scheduled maintenance is performed. You must submit a separate request each time you plan to bypass the control device, and your request must include the information specified in paragraphs (e)(1)(i) through (vi) of this section.

(i) Reason for the scheduled maintenance.

(ii) Explanation for why the maintenance cannot be performed when the kiln is shut down.

(iii) Detailed description of the maintenance activities.

(iv) Time required to complete the maintenance.

(v) How you will minimize HAP emissions from the kiln during the period when the control device is out of service.

(vi) How you will minimize the time when the kiln is operating and the control device is out of service for scheduled maintenance.

(2) You must minimize HAP emissions during the period when the kiln is operating and the control device is out of service.

(3) You must minimize the time period during which the kiln is operating and the control device is out of service.

(f) You must be in compliance with the provisions of subpart A of this part, except as noted in Table 11 to this subpart.

[68 FR 18747, Apr. 16, 2003, as amended at 71 FR 20471, Apr. 20, 2006]

§ 63.9794 What do I need to know about operation, maintenance, and monitoring plans?

(a) For each continuous parameter monitoring system (CPMS) required by this subpart, you must develop, imple-

ment, make available for inspection, and revise, as necessary, an OM&M plan that includes the information in paragraphs (a)(1) through (13) of this section.

(1) A list and identification of each process and add-on APCD that is required by this subpart to be monitored, the type of monitoring device that will be used, and the operating parameters that will be monitored.

(2) Specifications for the sensor, signal analyzer, and data collection system.

(3) A monitoring schedule that specifies the frequency that the parameter values will be determined and recorded.

(4) The operating limits for each parameter that represent continuous compliance with the emission limitations in § 63.9788, based on values of the monitored parameters recorded during performance tests.

(5) Procedures for installing the CPMS at a measurement location relative to each process unit or APCD such that measurement is representative of control of emissions.

(6) Procedures for the proper operation and routine and long-term maintenance of each process unit and APCD, including a maintenance and inspection schedule that is consistent with the manufacturer's recommendations.

(7) Procedures for the proper operation and maintenance of monitoring equipment consistent with the requirements in §§ 63.8(c)(1), (3), (4)(ii), (7), and (8), and 63.9804.

(8) Ongoing data quality assurance procedures in accordance with the general requirements of § 63.8(d).

(9) Procedures for evaluating the performance of each CPMS.

(10) Procedures for responding to operating parameter deviations, including the procedures in paragraphs (a)(10)(i) through (iii) of this section:

(i) Procedures for determining the cause of the operating parameter deviation.

(ii) Actions for correcting the deviation and returning the operating parameters to the allowable limits.

(iii) Procedures for recording the times that the deviation began and ended, and when corrective actions were initiated and completed.

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(11) Procedures for keeping records to document compliance and reporting in accordance with the requirements of § 63.10(c), (e)(1), and (e)(2)(i).

(12) If you operate a kiln that is subject to the limits on the type of fuel used, as specified in items 3 and 4 of Table 3 to subpart SSSSS, procedures for using alternative fuels.

(13) If you operate an affected continuous kiln and you plan to take the kiln control device out of service for scheduled maintenance, as specified in § 63.9792(e), the procedures specified in paragraphs (a)(13)(i) and (ii) of this section.

(i) Procedures for minimizing HAP emissions from the kiln during periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service.

(ii) Procedures for minimizing any period of scheduled maintenance on the kiln control device when the kiln is operating and the control device is out of service.

(b) Changes to the operating limits in your OM&M plan require a new performance test. If you are revising an operating limit parameter value, you must meet the requirements in paragraphs (b)(1) and (2) of this section.

(1) Submit a Notification of Performance Test to the Administrator as specified in § 63.7(b).

(2) After completing the performance tests to demonstrate that compliance with the emission limits can be achieved at the revised operating limit parameter value, you must submit the performance test results and the revised operating limits as part of the Notification of Compliance Status required under § 63.9(h).

(c) If you are revising the inspection and maintenance procedures in your OM&M plan, you do not need to conduct a new performance test.

TESTING AND INITIAL COMPLIANCE REQUIREMENTS

§ 63.9796 By what date must I conduct performance tests?

You must conduct performance tests within 180 calendar days after the compliance date that is specified for your

source in § 63.9786 and according to the provisions in § 63.7(a)(2).

§ 63.9798 When must I conduct subsequent performance tests?

(a) You must conduct a performance test every 5 years following the initial performance test, as part of renewing your 40 CFR part 70 or 40 CFR part 71 operating permit.

(b) You must conduct a performance test when you want to change the parameter value for any operating limit specified in your OM&M plan.

(c) If you own or operate a source that is subject to the emission limits specified in items 2 through 9 of Table 1 to this subpart, you must conduct a performance test on the source(s) listed in paragraphs (c)(1) and (2) of this section before you start production of any refractory product for which the organic HAP processing rate is likely to exceed by more than 10 percent the maximum organic HAP processing rate established during the most recent performance test on that same source.

(1) Each affected shape dryer or curing oven that is used to process the refractory product with the higher organic HAP processing rate.

(2) Each affected kiln that follows an affected shape dryer or curing oven and is used to process the refractory product with the higher organic HAP processing rate.

(d) If you own or operate a kiln that is subject to the emission limits specified in item 5 or 9 of Table 1 to this subpart, you must conduct a performance test on the affected kiln following any process changes that are likely to increase organic HAP emissions from the kiln (e.g., a decrease in the curing cycle time for a curing oven that precedes the affected kiln in the process line).

(e) If you own or operate a clay refractory products kiln that is subject to the emission limits specified in item 10 or 11 of Table 1 to this subpart and is controlled with a dry limestone adsorber (DLA), you must conduct a performance test on the affected kiln following any change in the source of limestone used in the DLA.

§ 63.9800 How do I conduct performance tests and establish operating limits?

(a) You must conduct each performance test in Table 4 to this subpart that applies to you.

(b) Before conducting the performance test, you must install and validate all monitoring equipment.

(c) Each performance test must be conducted according to the requirements in § 63.7 and under the specific conditions in Table 4 to this subpart.

(d) You may not conduct performance tests during periods of startup, shutdown, or malfunction, as specified in § 63.7(e)(1).

(e) You must conduct separate test runs for at least the duration specified for each performance test required in this section, as specified in § 63.7(e)(3) and Table 4 to this subpart.

(f) For batch process sources, you must satisfy the requirements specified in paragraphs (f)(1) through (5) of this section.

(1) You must conduct at least two test runs.

(2) Each test run must last an entire batch cycle unless you develop an emissions profile, as specified in items 8(a)(i)(4) and 17(b)(i)(4) of Table 4 to this subpart, or you satisfy the conditions for terminating a test run prior to the completion of a batch cycle as specified in item 8(a)(i)(5) of Table 4 to this subpart.

(3) Each test run must be performed over a separate batch cycle unless you satisfy the conditions for conducting both test runs over a single batch cycle, as described in paragraphs (f)(3)(i) and (ii) of this section.

(i) You do not produce the product that corresponds to the maximum organic HAP processing rate for that batch process source in consecutive batch cycles.

(ii) To produce that product in two consecutive batch cycles would disrupt production of other refractory products.

(4) If you want to conduct a performance test over a single batch cycle, you must include in your Notification of Performance Test the rationale for testing over a single batch cycle.

(5) If you are granted approval to conduct a performance test over a sin-

gle batch cycle, you must use paired sampling trains and collect two sets of emissions data. Each set of data can be considered a separate test run.

(g) You must use the data gathered during the performance test and the equations in paragraphs (g)(1) through (3) of this section to determine compliance with the emission limitations.

(1) To determine compliance with the total hydrocarbon (THC) emission concentration limit listed in Table 1 to this subpart, you must calculate your emission concentration corrected to 18 percent oxygen for each test run using Equation 1 of this section:

$$C_{\text{THC-C}} = \frac{2.9 \times C_{\text{THC}}}{(20.9 - C_{\text{O}_2})} \quad (\text{Eq. 1})$$

Where:

$C_{\text{THC-C}}$ = THC concentration, corrected to 18 percent oxygen, parts per million by volume, dry basis (ppmvd)

C_{THC} = THC concentration (uncorrected), ppmvd

C_{O_2} = oxygen concentration, percent.

(2) To determine compliance with any of the emission limits based on percentage reduction across an emissions control system specified in Table 1 to this subpart, you must calculate the percentage reduction for each test run using Equation 2 of this section:

$$\text{PR} = \frac{\text{ER}_i - \text{ER}_o}{\text{ER}_i} \times 100 \quad (\text{Eq. 2})$$

Where:

PR = percentage reduction, percent

ER_i = mass emissions rate of specific HAP or pollutant (THC, HF, or HCl) entering the control device, kilograms (pounds) per hour

ER_o = mass emissions rate of specific HAP or pollutant (THC, HF, or HCl) exiting the control device, kilograms (pounds) per hour.

(3) To determine compliance with production-based hydrogen fluoride (HF) and hydrogen chloride (HCl) emission limits in Table 1 to this subpart, you must calculate your mass emissions per unit of uncalcined clay processed for each test run using Equation 3 of this section:

$$\text{MP} = \frac{\text{ER}}{\text{P}} \quad (\text{Eq. 3})$$

Where:

MP = mass per unit of production, kilograms of pollutant per megagram (pounds per ton) of uncalcined clay processed

ER = mass emissions rate of specific HAP (HF or HCl) during each performance test run, kilograms (pounds) per hour

P = average uncalcined clay processing rate for the performance test, megagrams (tons) of uncalcined clay processed per hour.

(h) You must establish each site-specific operating limit in Table 2 to this subpart that applies to you, as specified in Table 4 to this subpart.

(i) For each affected source that is equipped with an add-on APCD that is not addressed in Table 2 to this subpart or that is using process changes as a means of meeting the emission limits in Table 1 to this subpart, you must meet the requirements in §63.8(f) and paragraphs (i)(1) through (3) of this section.

(1) For sources subject to the THC concentration limit specified in item 3 or 7 of Table 1 to this subpart, you must satisfy the requirements specified in paragraphs (i)(1)(i) through (iii) of this section.

(i) You must install a THC continuous emissions monitoring system (CEMS) at the outlet of the control device or in the stack of the affected source.

(ii) You must meet the requirements specified in Performance Specification (PS) 8 of 40 CFR part 60, appendix B.

(iii) You must meet the requirements specified in Procedure 1 of 40 CFR part 60, appendix F.

(2) For sources subject to the emission limits specified in item 3, 4, 7, or 8 of Table 1 to this subpart, you must submit a request for approval of alternative monitoring methods to the Administrator no later than the submittal date for the Notification of Performance Test, as specified in §63.9812(d). The request must contain the information specified in paragraphs (i)(2)(i) through (v) of this section.

(i) Description of the alternative add-on APCD or process changes.

(ii) Type of monitoring device or method that will be used, including the sensor type, location, inspection procedures, quality assurance and quality control measures, and data recording device.

(iii) Operating parameters that will be monitored.

(iv) Frequency that the operating parameter values will be determined and recorded to establish continuous compliance with the operating limits.

(v) Averaging time.

(3) You must establish site-specific operating limits during the performance test based on the information included in the approved alternative monitoring methods request and, as applicable, as specified in Table 4 to this subpart.

§ 63.9802 How do I develop an emissions profile?

If you decide to develop an emissions profile for an affected batch process source; as indicated in item 8(a)(i)(4) or 17(b)(i)(4) of Table 4 to this subpart, you must measure and record mass emissions of the applicable pollutant throughout a complete batch cycle of the affected batch process source according to the procedures described in paragraph (a) or (b) of this section.

(a) If your affected batch process source is subject to the THC concentration limit specified in item 6(a), 7(a), 8, or 9 of Table 1 to this subpart or the THC percentage reduction limit specified in item 6(b) or 7(b) of Table 1 to this subpart, you must measure and record the THC mass emissions rate at the inlet to the control device using the test methods, averaging periods, and procedures specified in items 10(a) and (b) of Table 4 to this subpart for each complete hour of the batch process cycle.

(b) If your affected batch process source is subject to the HF and HCl percentage reduction emission limits in item 11 of Table 1 to this subpart, you must measure and record the HF mass emissions rate at the inlet to the control device through a series of 1-hour test runs according to the test method specified in item 14(a) of Table 4 to this subpart for each complete hour of the batch process cycle.

§ 63.9804 What are my monitoring system installation, operation, and maintenance requirements?

(a) You must install, operate, and maintain each CPMS required by this subpart according to your OM&M plan

and the requirements in paragraphs (a)(1) through (15) of this section.

(1) You must satisfy all applicable requirements of performance specifications for CPMS specified in 40 CFR part 60, appendix B, upon promulgation of such performance specifications.

(2) You must satisfy all applicable requirements of quality assurance (QA) procedures for CPMS specified in 40 CFR part 60, appendix F, upon promulgation of such QA procedures.

(3) You must install each sensor of your CPMS in a location that provides representative measurement of the appropriate parameter over all operating conditions, taking into account the manufacturer's guidelines.

(4) You must use a CPMS that is capable of measuring the appropriate parameter over a range that extends from a value of at least 20 percent less than the lowest value that you expect your CPMS to measure, to a value of at least 20 percent greater than the highest value that you expect your CPMS to measure.

(5) You must use a data acquisition and recording system that is capable of recording values over the entire range specified in paragraph (a)(4) of this section.

(6) You must use a signal conditioner, wiring, power supply, and data acquisition and recording system that are compatible with the output signal of the sensors used in your CPMS.

(7) You must perform an initial calibration of your CPMS based on the procedures specified in the manufacturer's owner's manual.

(8) You must use a CPMS that is designed to complete a minimum of one cycle of operation for each successive 15-minute period. To have a valid hour of data, you must have at least three of four equally-spaced data values (or at least 75 percent of the total number of values if you collect more than four data values per hour) for that hour (not including startup, shutdown, malfunction, or out-of-control periods).

(9) You must record valid data from at least 90 percent of the hours during which the affected source or process operates.

(10) You must determine and record the 15-minute block averages of all measurements, calculated after every

15 minutes of operation as the average of the previous 15 operating minutes (not including periods of startup, shutdown, or malfunction).

(11) You must determine and record the 3-hour block averages of all 15-minute recorded measurements, calculated after every 3 hours of operation as the average of the previous 3 operating hours (not including periods of startup, shutdown, or malfunction).

(12) You must record the results of each inspection, calibration, initial validation, and accuracy audit.

(13) At all times, you must maintain your CPMS including, but not limited to, maintaining necessary parts for routine repairs of the CPMS.

(14) You must perform an initial validation of your CPMS under the conditions specified in paragraphs (14)(i) and (ii) of this section.

(i) Prior to the initial performance test on the affected source for which the CPMS is required.

(ii) Within 180 days of your replacing or relocating one or more of the sensors of your CPMS.

(15) Except for redundant sensors, as defined in § 63.9824, any device that you use to conduct an initial validation or accuracy audit of your CPMS must meet the accuracy requirements specified in paragraphs (15)(i) and (ii) of this section.

(i) The device must have an accuracy that is traceable to National Institute of Standards and Technology (NIST) standards.

(ii) The device must be at least three times as accurate as the required accuracy for the CPMS.

(b) For each temperature CPMS that is used to monitor the combustion chamber temperature of a thermal oxidizer or the catalyst bed inlet temperature of a catalytic oxidizer, you must meet the requirements in paragraphs (a) and (b)(1) through (6) of this section.

(1) Use a temperature CPMS with a minimum accuracy of ± 1.0 percent of the temperature value or 2.8 degrees Celsius ($^{\circ}\text{C}$) (5 degrees Fahrenheit ($^{\circ}\text{F}$)), whichever is greater.

(2) Use a data recording system with a minimum resolution of one-half or better of the required CPMS accuracy

specified in paragraph (b)(1) of this section.

(3) Perform an initial validation of your CPMS according to the requirements in paragraph (3)(i) or (ii) of this section.

(i) Place the sensor of a calibrated temperature measurement device adjacent to the sensor of your temperature CPMS in a location that is subject to the same environment as the sensor of your temperature CPMS. The calibrated temperature measurement device must satisfy the accuracy requirements of paragraph (a)(15) of this section. While the process and control device that is monitored by your CPMS are operating normally, record concurrently and compare the temperatures measured by your temperature CPMS and the calibrated temperature measurement device. Using the calibrated temperature measurement device as the reference, the temperature measured by your CPMS must be within the accuracy specified in paragraph (b)(1) of this section.

(ii) Perform any of the initial validation methods for temperature CPMS specified in performance specifications for CPMS established in 40 CFR part 60, appendix B.

(4) Perform an accuracy audit of your temperature CPMS at least quarterly, according to the requirements in paragraph (b)(4)(i), (ii), or (iii) of this section.

(i) If your temperature CPMS includes a redundant temperature sensor, record three pairs of concurrent temperature measurements within a 24-hour period. Each pair of concurrent measurements must consist of a temperature measurement by each of the two temperature sensors. The minimum time interval between any two such pairs of consecutive temperature measurements is 1 hour. The measurements must be taken during periods when the process and control device that is monitored by your temperature CPMS are operating normally. Calculate the mean of the three values for each temperature sensor. The mean values must agree within the required overall accuracy of the CPMS, as specified in paragraph (b)(1) of this section.

(ii) If your temperature CPMS does not include a redundant temperature

sensor, place the sensor of a calibrated temperature measurement device adjacent to the sensor of your temperature CPMS in a location that is subject to the same environment as the sensor of your temperature CPMS. The calibrated temperature measurement device must satisfy the accuracy requirements of paragraph (a)(15) of this section. While the process and control device that is monitored by your temperature CPMS are operating normally, record concurrently and compare the temperatures measured by your CPMS and the calibrated temperature measurement device. Using the calibrated temperature measurement device as the reference, the temperature measured by your CPMS must be within the accuracy specified in paragraph (b)(1) of this section.

(iii) Perform any of the accuracy audit methods for temperature CPMS specified in QA procedures for CPMS established in 40 CFR part 60, appendix F.

(5) Conduct an accuracy audit of your CPMS following any 24-hour period throughout which the temperature measured by your CPMS exceeds the manufacturer's specified maximum operating temperature range, or install a new temperature sensor.

(6) If your CPMS is not equipped with a redundant temperature sensor, perform at least quarterly a visual inspection of all components of the CPMS for integrity, oxidation, and galvanic corrosion.

(c) For each pressure CPMS that is used to monitor the pressure drop across a DLA or wet scrubber, you must meet the requirements in paragraphs (a) and (c)(1) through (7) of this section.

(1) Use a pressure CPMS with a minimum accuracy of ± 5.0 percent or 0.12 kilopascals (kPa) (0.5 inches of water column (in. w.c.)), whichever is greater.

(2) Use a data recording system with a minimum resolution of one-half the required CPMS accuracy specified in paragraph (c)(1) of this section, or better.

(3) Perform an initial validation of your pressure CPMS according to the requirements in paragraph (c)(3)(i) or (ii) of this section.

(i) Place the sensor of a calibrated pressure measurement device adjacent to the sensor of your pressure CPMS in a location that is subject to the same environment as the sensor of your pressure CPMS. The calibrated pressure measurement device must satisfy the accuracy requirements of paragraph (a)(15) of this section. While the process and control device that is monitored by your CPMS are operating normally, record concurrently and compare the pressure measured by your CPMS and the calibrated pressure measurement device. Using the calibrated pressure measurement device as the reference, the pressure measured by your CPMS must be within the accuracy specified in paragraph (c)(1) of this section.

(ii) Perform any of the initial validation methods for pressure CPMS specified in performance specifications for CPMS established in 40 CFR part 60, appendix B.

(4) Perform an accuracy audit of your pressure CPMS at least quarterly, according to the requirements in paragraph (c)(4)(i), (ii), or (iii) of this section.

(i) If your pressure CPMS includes a redundant pressure sensor, record three pairs of concurrent pressure measurements within a 24-hour period. Each pair of concurrent measurements must consist of a pressure measurement by each of the two pressure sensors. The minimum time interval between any two such pairs of consecutive pressure measurements is 1 hour. The measurements must be taken during periods when the process and control device that is monitored by your CPMS are operating normally. Calculate the mean of the three pressure measurement values for each pressure sensor. The mean values must agree within the required overall accuracy of the CPMS, as specified in paragraph (c)(1) of this section.

(ii) If your pressure CPMS does not include a redundant pressure sensor, place the sensor of a calibrated pressure measurement device adjacent to the sensor of your pressure CPMS in a location that is subject to the same environment as the sensor of your pressure CPMS. The calibrated pressure measurement device must satisfy the accuracy requirements of paragraph

(a)(15) of this section. While the process and control device that is monitored by your pressure CPMS are operating normally, record concurrently and compare the pressure measured by your CPMS and the calibrated pressure measurement device. Using the calibrated pressure measurement device as the reference, the pressure measured by your CPMS must be within the accuracy specified in paragraph (c)(1) of this section.

(iii) Perform any of the accuracy audit methods for pressure CPMS specified in QA procedures for CPMS established in 40 CFR part 60, appendix F.

(5) Conduct an accuracy audit of your CPMS following any 24-hour period throughout which the pressure measured by your CPMS exceeds the manufacturer's specified maximum operating pressure range, or install a new pressure sensor.

(6) At least monthly, check all mechanical connections on your CPMS for leakage.

(7) If your CPMS is not equipped with a redundant pressure sensor, perform at least quarterly a visual inspection of all components of the CPMS for integrity, oxidation, and galvanic corrosion.

(d) For each liquid flow rate CPMS that is used to monitor the liquid flow rate in a wet scrubber, you must meet the requirements in paragraphs (a) and (d)(1) through (7) of this section.

(1) Use a flow rate CPMS with a minimum accuracy of ± 5.0 percent or 1.9 liters per minute (L/min) (0.5 gallons per minute (gal/min)), whichever is greater.

(2) Use a data recording system with a minimum resolution of one-half the required CPMS accuracy specified in paragraph (d)(1) of this section, or better.

(3) Perform an initial validation of your CPMS according to the requirements in paragraph (3)(i) or (ii) of this section.

(i) Use a calibrated flow rate measurement system to measure the liquid flow rate in a location that is adjacent to the measurement location for your flow rate CPMS and is subject to the same environment as your flow rate CPMS. The calibrated flow rate measurement device must satisfy the accuracy requirements of paragraph (a)(15)

of this section. While the process and control device that is monitored by your flow rate CPMS are operating normally, record concurrently and compare the flow rates measured by your flow rate CPMS and the calibrated flow rate measurement device. Using the calibrated flow rate measurement device as the reference, the flow rate measured by your CPMS must be within the accuracy specified in paragraph (d)(1) of this section.

(ii) Perform any of the initial validation methods for liquid flow rate CPMS specified in performance specifications for CPMS established in 40 CFR part 60, appendix B.

(4) Perform an accuracy audit of your flow rate CPMS at least quarterly, according to the requirements in paragraph (d)(4)(i), (ii), or (iii) of this section.

(i) If your flow rate CPMS includes a redundant sensor, record three pairs of concurrent flow rate measurements within a 24-hour period. Each pair of concurrent measurements must consist of a flow rate measurement by each of the two flow rate sensors. The minimum time interval between any two such pairs of consecutive flow rate measurements is 1 hour. The measurements must be taken during periods when the process and control device that is monitored by your flow rate CPMS are operating normally. Calculate the mean of the three flow rate measurement values for each flow rate sensor. The mean values must agree within the required overall accuracy of the CPMS, as specified in paragraph (d)(1) of this section.

(ii) If your flow rate CPMS does not include a redundant flow rate sensor, place the sensor of a calibrated flow rate measurement device adjacent to the sensor of your flow rate CPMS in a location that is subject to the same environment as the sensor of your flow rate CPMS. The calibrated flow rate measurement device must satisfy the accuracy requirements of paragraph (a)(15) of this section. While the process and control device that is monitored by your flow rate CPMS are operating normally, record concurrently and compare the flow rate measured by your pressure CPMS and the calibrated flow rate measurement device. Using

the calibrated flow rate measurement device as the reference, the flow rate measured by your CPMS must be within the accuracy specified in paragraph (d)(1) of this section.

(iii) Perform any of the accuracy audit methods for liquid flow rate CPMS specified in QA procedures for CPMS established in 40 CFR part 60, appendix F.

(5) Conduct an accuracy audit of your flow rate CPMS following any 24-hour period throughout which the flow rate measured by your CPMS exceeds the manufacturer's specified maximum operating range, or install a new flow rate sensor.

(6) At least monthly, check all mechanical connections on your CPMS for leakage.

(7) If your CPMS is not equipped with a redundant flow rate sensor, perform at least quarterly a visual inspection of all components of the CPMS for integrity, oxidation, and galvanic corrosion.

(e) For each pH CPMS that is used to monitor the pH of a wet scrubber liquid, you must meet the requirements in paragraphs (a) and (e)(1) through (5) of this section.

(1) Use a pH CPMS with a minimum accuracy of ± 0.2 pH units.

(2) Use a data recording system with a minimum resolution of 0.1 pH units, or better.

(3) Perform an initial validation of your pH CPMS according to the requirements in paragraph (e)(3)(i) or (ii) of this section.

(i) Perform a single-point calibration using an NIST-certified buffer solution that is accurate to within ± 0.02 pH units at 25 °C (77 °F). If the expected pH of the liquid that is monitored lies in the acidic range (less than 7 pH), use a buffer solution with a pH value of 4.00. If the expected pH of the liquid that is monitored is neutral or lies in the basic range (equal to or greater than 7 pH), use a buffer solution with a pH value of 10.00. Place the electrode of your pH CPMS in the container of buffer solution. Record the pH measured by your CPMS. Using the certified buffer solution as the reference, the pH measured by your CPMS must be within the accuracy specified in paragraph (e)(1) of this section.

(ii) Perform any of the initial validation methods for pH CPMS specified in performance specifications for CPMS established in 40 CFR part 60, appendix B.

(4) Perform an accuracy audit of your pH CPMS at least weekly, according to the requirements in paragraph (e)(4)(i), (ii), or (iii) of this section.

(i) If your pH CPMS includes a redundant pH sensor, record the pH measured by each of the two pH sensors. The measurements must be taken during periods when the process and control device that is monitored by your pH CPMS are operating normally. The two pH values must agree within the required overall accuracy of the CPMS, as specified in paragraph (e)(1) of this section.

(ii) If your pH CPMS does not include a redundant pH sensor, perform a single point calibration using an NIST-certified buffer solution that is accurate to within ± 0.02 pH units at 25 °C (77 °F). If the expected pH of the liquid that is monitored lies in the acidic range (less than 7 pH), use a buffer solution with a pH value of 4.00. If the expected pH of the liquid that is monitored is neutral or lies in the basic range (equal to or greater than 7 pH), use a buffer solution with a pH value of 10.00. Place the electrode of the pH CPMS in the container of buffer solution. Record the pH measured by your CPMS. Using the certified buffer solution as the reference, the pH measured by your CPMS must be within the accuracy specified in paragraph (e)(1) of this section.

(iii) Perform any of the accuracy audit methods for pH CPMS specified in QA procedures for CPMS established in 40 CFR part 60, appendix F.

(5) If your CPMS is not equipped with a redundant pH sensor, perform at least monthly a visual inspection of all components of the CPMS for integrity, oxidation, and galvanic corrosion.

(f) For each bag leak detection system, you must meet the requirements in paragraphs (f)(1) through (11) of this section.

(1) Each triboelectric bag leak detection system must be installed, calibrated, operated, and maintained according to the "Fabric Filter Bag Leak Detection Guidance" (EPA-454/R-98-

015, September 1997). That document is available from the U.S. EPA; Office of Air Quality Planning and Standards; Emissions, Monitoring and Analysis Division; Emission Measurement Center (D205-02), Research Triangle Park, NC 27711. It is also available on the Technology Transfer Network (TTN) at the following address: <http://www.epa.gov/ttn/emc/cem.html>. Other types of bag leak detection systems must be installed, operated, calibrated, and maintained in a manner consistent with the manufacturer's written specifications and recommendations.

(2) The bag leak detection system must be certified by the manufacturer to be capable of detecting particulate matter (PM) emissions at concentrations of 10 milligrams per actual cubic meter (0.0044 grains per actual cubic foot) or less.

(3) The bag leak detection system sensor must provide an output of relative PM loadings.

(4) The bag leak detection system must be equipped with a device to continuously record the output signal from the sensor.

(5) The bag leak detection system must be equipped with an alarm system that will be engaged automatically when an increase in relative PM emissions over a preset level is detected. The alarm must be located where it is easily recognized by plant operating personnel.

(6) For positive pressure fabric filter systems, a bag leak detector must be installed in each baghouse compartment or cell.

(7) For negative pressure or induced air fabric filters, the bag leak detector must be installed downstream of the fabric filter.

(8) Where multiple detectors are required, the system's instrumentation and alarm may be shared among detectors.

(9) The baseline output must be established by adjusting the range and the averaging period of the device and establishing the alarm set points and the alarm delay time according to section 5.0 of the "Fabric Filter Bag Leak Detection Guidance."

(10) Following initial adjustment of the system, the owner or operator must not adjust the sensitivity or

range, averaging period, alarm set points, or alarm delay time except as detailed in the OM&M plan. In no case may the sensitivity be increased by more than 100 percent or decreased by more than 50 percent over a 365-day period unless such adjustment follows a complete fabric filter inspection that demonstrates that the fabric filter is in good operating condition. You must record each adjustment of your bag leak detection system.

(11) Record the results of each inspection, calibration, and validation check.

(g) For each lime feed rate measurement device that is used to monitor the lime feed rate of a dry injection fabric filter (DIFF) or dry lime scrubber/fabric filter (DLS/FF), or the chemical feed rate of a wet scrubber, you must meet the requirements in paragraph (a) of this section.

(h) For each affected source that is subject to the emission limit specified in item 3, 4, 7, or 8 of Table 1 to this subpart, you must satisfy the requirements of paragraphs (h)(1) through (3) of this section.

(1) Install a THC CEMS at the outlet of the control device or in the stack of the affected source.

(2) Meet the requirements of PS-8 of 40 CFR part 60, appendix B.

(3) Meet the requirements of Procedure 1 of 40 CFR part 60, appendix F.

(i) Requests for approval of alternate monitoring methods must meet the requirements in §§ 63.9800(1)(2) and 63.8(f).

§ 63.9806 How do I demonstrate initial compliance with the emission limits, operating limits, and work practice standards?

(a) You must demonstrate initial compliance with each emission limit that applies to you according to the requirements specified in Table 5 to this subpart.

(b) You must establish each site-specific operating limit in Table 2 to this subpart that applies to you according to the requirements specified in § 63.9800 and Table 4 to this subpart.

(c) You must demonstrate initial compliance with each work practice standard that applies to you according to the requirements specified in Table 6 to this subpart.

(d) You must submit the Notification of Compliance Status containing the

results of the initial compliance demonstration according to the requirements in § 63.9812(e).

CONTINUOUS COMPLIANCE REQUIREMENTS

§ 63.9808 How do I monitor and collect data to demonstrate continuous compliance?

(a) You must monitor and collect data according to this section.

(b) At all times, you must maintain your monitoring systems including, but not limited to, maintaining necessary parts for routine repairs of the monitoring equipment.

(c) Except for, as applicable, monitoring system malfunctions, associated repairs, and required quality assurance or quality control activities, you must monitor continuously whenever your affected process unit is operating. For purposes of calculating data averages, you must not use data recorded during monitoring system malfunctions, associated repairs, and required quality assurance or quality control activities. You must use all the data collected during all other periods in assessing compliance. A monitoring system malfunction is any sudden, infrequent, not reasonably preventable failure of the monitoring system to provide valid data. Monitoring system malfunctions include out of control continuous monitoring systems (CMS), such as a CPMS. Any averaging period for which you do not have valid monitoring data as a result of a monitoring system malfunction and for which such data are required constitutes a deviation, and you must notify the Administrator in accordance with § 63.9814(e). Monitoring system failures are different from monitoring system malfunctions in that they are caused in part by poor maintenance or careless operation. Any period for which there is a monitoring system failure and data are not available for required calculations constitutes a deviation and you must notify the Administrator in accordance with § 63.9814(e).

§ 63.9810 How do I demonstrate continuous compliance with the emission limits, operating limits, and work practice standards?

(a) You must demonstrate continuous compliance with each emission

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limit specified in Table 1 to this subpart that applies to you according to the requirements specified in Table 7 to this subpart.

(b) You must demonstrate continuous compliance with each operating limit specified in Table 2 to this subpart that applies to you according to the requirements specified in Table 8 to this subpart.

(c) You must demonstrate continuous compliance with each work practice standard specified in Table 3 to this subpart that applies to you according to the requirements specified in Table 9 to this subpart.

(d) For each affected source that is equipped with an add-on APCD that is not addressed in Table 2 to this subpart or that is using process changes as a means of meeting the emission limits in Table 1 to this subpart, you must demonstrate continuous compliance with each emission limit in Table 1 to this subpart and each operating limit established as required in § 63.9800(i)(3) according to the methods specified in your approved alternative monitoring methods request as described in § 63.9800(i)(2).

(e) You must report each instance in which you did not meet each emission limit and each operating limit in this subpart that applies to you. This includes periods of startup, shutdown, and malfunction. These instances are deviations from the emission limitations in this subpart. These deviations must be reported according to the requirements in § 63.9814.

(1) [Reserved]

(2) Consistent with §§ 63.6(e) and 63.7(e)(1), deviations that occur during a period of startup, shutdown, or malfunction are not violations if you demonstrate to the Administrator's satisfaction that you were operating in accordance with § 63.6(e)(1) and your OM&M plan. The Administrator will determine whether deviations that occur during a period of startup, shutdown, or malfunction are violations, according to the provisions in § 63.6(e).

[68 FR 18747, Apr. 16, 2003, as amended at 71 FR 20471, Apr. 20, 2006]

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NOTIFICATIONS, REPORTS, AND RECORDS

§ 63.9812 What notifications must I submit and when?

(a) You must submit all of the notifications in §§ 63.7(b) and (c), 63.8(f)(4), and 63.9 (b) through (e) and (h) that apply to you by the dates specified.

(b) As specified in § 63.9(b)(2) and (3), if you start up your affected source before April 16, 2003, you must submit an Initial Notification not later than 120 calendar days after April 16, 2003.

(c) As specified in § 63.9(b)(3), if you start up your new or reconstructed affected source on or after April 16, 2003, you must submit an Initial Notification not later than 120 calendar days after you become subject to this subpart.

(d) If you are required to conduct a performance test, you must submit a Notification of Performance Test at least 60 calendar days before the performance test is scheduled to begin, as required in § 63.7(b)(1).

(e) If you are required to conduct a performance test, you must submit a Notification of Compliance Status as specified in § 63.9(h) and paragraphs (e)(1) and (2) of this section.

(1) For each compliance demonstration that includes a performance test conducted according to the requirements in Table 4 to this subpart, you must submit the Notification of Compliance Status, including the performance test results, before the close of business on the 60th calendar day following the completion of the performance test, according to § 63.10(d)(2).

(2) In addition to the requirements in § 63.9(h)(2)(i), you must include the information in paragraphs (e)(2)(i) through (iv) of this section in your Notification of Compliance Status.

(i) The operating limit parameter values established for each affected source with supporting documentation and a description of the procedure used to establish the values.

(ii) Design information and analysis with supporting documentation demonstrating conformance with requirements for capture/collection systems in Table 2 to this subpart.

(iii) A description of the methods used to comply with any applicable work practice standard.

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(iv) For each APCD that includes a fabric filter, analysis and supporting documentation demonstrating conformance with EPA guidance and specifications for bag leak detection systems in § 63.9804(f).

(f) If you operate a clay refractory products kiln or a chromium refractory products kiln that is subject to the work practice standard specified in item 3 or 4 of Table 3 to this subpart, and you intend to use a fuel other than natural gas or equivalent to fire the affected kiln, you must submit a notification of alternative fuel use within 48 hours of the declaration of a period of natural gas curtailment or supply interruption, as defined in § 63.9824. The notification must include the information specified in paragraphs (f)(1) through (5) of this section.

(1) Company name and address.

(2) Identification of the affected kiln.

(3) Reason you are unable to use natural gas or equivalent fuel, including the date when the natural gas curtailment was declared or the natural gas supply interruption began.

(4) Type of alternative fuel that you intend to use.

(5) Dates when the alternative fuel use is expected to begin and end.

(g) If you own or operate an affected continuous kiln and must perform scheduled maintenance on the control device for that kiln, you must request approval from the Administrator before bypassing the control device, as specified in § 63.9792(e). You must submit a separate request for approval each time you plan to bypass the kiln control device.

§ 63.9814 What reports must I submit and when?

(a) You must submit each report in Table 10 to this subpart that applies to you.

(b) Unless the Administrator has approved a different schedule for submission of reports under § 63.10(a), you must submit each report by the date in Table 10 to this subpart and as specified in paragraphs (b)(1) through (5) of this section.

(1) The first compliance report must cover the period beginning on the compliance date that is specified for your affected source in § 63.9786 and ending

on June 30 or December 31 and lasting at least 6 months but less than 12 months. For example, if your compliance date is March 1, then the first semiannual reporting period would begin on March 1 and end on December 31.

(2) The first compliance report must be postmarked or delivered no later than July 31 or January 31 for compliance periods ending on June 30 and December 31, respectively.

(3) Each subsequent compliance report must cover the semiannual reporting period from January 1 through June 30 or the semiannual reporting period from July 1 through December 31.

(4) Each subsequent compliance report must be postmarked or delivered no later than July 31 or January 31 for compliance periods ending on June 30 and December 31, respectively.

(5) For each affected source that is subject to permitting regulations pursuant to 40 CFR part 70 or 40 CFR part 71 and, if the permitting authority has established dates for submitting semiannual reports pursuant to 40 CFR 70.6(a)(3)(iii)(A) or 40 CFR 71.6(a)(3)(iii)(A), you may submit the first and subsequent compliance reports according to the dates the permitting authority has established instead of according to the dates in paragraphs (b)(1) through (4) of this section. In such cases, you must notify the Administrator of this change.

(c) The compliance report must contain the information in paragraphs (c)(1) through (6) of this section.

(1) Company name and address.

(2) Statement by a responsible official with that official's name, title, and signature, certifying that, based on information and belief formed after reasonable inquiry, the statements and information in the report are true, accurate, and complete.

(3) Date of report and beginning and ending dates of the reporting period.

(4) If you had a startup, shutdown, or malfunction during the reporting period, and you took actions consistent with your SSMP and OM&M plan, the compliance report must include the information specified in § 63.10(d)(5)(i).

(5) If there are no deviations from any emission limitations (emission

limit, operating limit, or work practice standard) that apply to you, the compliance report must include a statement that there were no deviations from the emission limitations during the reporting period.

(6) If there were no periods during which any affected CPMS was out of control as specified in § 63.8(c)(7), the compliance report must include a statement that there were no periods during which the CPMS was out of control during the reporting period.

(d) For each deviation from an emission limitation (emission limit, operating limit, or work practice standard) that occurs at an affected source where you are not using a CPMS to comply with the emission limitations in this subpart, the compliance report must contain the information in paragraphs (c)(1) through (4) and (d)(1) and (2) of this section. This includes periods of startup, shutdown, and malfunction.

(1) The compliance report must include the total operating time of each affected source during the reporting period.

(2) The compliance report must include information on the number, duration, and cause of deviations (including unknown cause, if applicable) and the corrective action taken.

(e) For each deviation from an emission limitation (emission limit, operating limit, or work practice standard) occurring at an affected source where you are using a CPMS to comply with the emission limitation in this subpart, the compliance report must include the information in paragraphs (c)(1) through (4) and (e)(1) through (13) of this section. This includes periods of startup, shutdown, and malfunction.

(1) The total operating time of each affected source during the reporting period.

(2) The date and time that each startup, shutdown, or malfunction started and stopped.

(3) The date, time, and duration that each CPMS was inoperative.

(4) The date, time and duration that each CPMS was out of control, including the information in § 63.8(c)(8), as required by your OM&M plan.

(5) The date and time that each deviation from an emission limitation (emission limit, operating limit, or

work practice standard) started and stopped, and whether each deviation occurred during a period of startup, shutdown, or malfunction.

(6) A description of corrective action taken in response to a deviation.

(7) A summary of the total duration of the deviations during the reporting period and the total duration as a percentage of the total source operating time during that reporting period.

(8) A breakdown of the total duration of the deviations during the reporting period into those that are due to startup, shutdown, control equipment problems, process problems, other known causes, and other unknown causes.

(9) A summary of the total duration of CPMS downtime during the reporting period and the total duration of CPMS downtime as a percentage of the total source operating time during that reporting period.

(10) A brief description of the process units.

(11) A brief description of the CPMS.

(12) The date of the latest CPMS initial validation or accuracy audit.

(13) A description of any changes in CPMS, processes, or controls since the last reporting period.

(f) If you have obtained a title V operating permit pursuant to 40 CFR part 70 or 40 CFR part 71, you must report all deviations as defined in this subpart in the semiannual monitoring report required by 40 CFR 70.6(a)(3)(iii)(A) or 40 CFR 71.6(a)(3)(iii)(A). If you submit a compliance report according to Table 10 to this subpart along with, or as part of, the semiannual monitoring report required by 40 CFR 70.6(a)(3)(iii)(A) or 40 CFR 71.6(a)(3)(iii)(A), and the compliance report includes all required information concerning deviations from any emission limitation (including any operating limit), then submitting the compliance report will satisfy any obligation to report the same deviations in the semiannual monitoring report. However, submitting a compliance report will not otherwise affect any obligation you may have to report deviations from permit requirements to the permit authority.

(g) If you operate a clay refractory products kiln or a chromium refractory products kiln that is subject to the work practice standard specified in

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item 3 or 4 of Table 3 to this subpart, and you use a fuel other than natural gas or equivalent to fire the affected kiln, you must submit a report of alternative fuel use within 10 working days after terminating the use of the alternative fuel. The report must include the information in paragraphs (g)(1) through (6) of this section.

- (1) Company name and address.
- (2) Identification of the affected kiln.
- (3) Reason for using the alternative fuel.
- (4) Type of alternative fuel used to fire the affected kiln.
- (5) Dates that the use of the alternative fuel started and ended.
- (6) Amount of alternative fuel used.

§ 63.9816 What records must I keep?

(a) You must keep the records listed in paragraphs (a)(1) through (3) of this section.

(1) A copy of each notification and report that you submitted to comply with this subpart, including all documentation supporting any Initial Notification or Notification of Compliance Status that you submitted, according to the requirements in § 63.10(b)(2)(xiv).

(2) The records in § 63.6(e)(3)(iii) through (v) related to startup, shutdown, and malfunction.

(3) Records of performance tests as required in § 63.10(b)(2)(viii).

(b) You must keep the records required in Tables 7 through 9 to this subpart to show continuous compliance with each emission limitation that applies to you.

(c) You must also maintain the records listed in paragraphs (c)(1) through (10) of this section.

(1) Records of emission data used to develop an emissions profile, as indicated in items 8(a)(1)(4) and 17(b)(1)(4) of Table 4 to this subpart.

(2) Records that document how you comply with any applicable work practice standard.

(3) For each bag leak detection system, records of each alarm, the time of the alarm, the time corrective action was initiated and completed, and a brief description of the cause of the alarm and the corrective action taken.

(4) For each kiln controlled with a DLA, records that document the source of limestone used.

(5) For each deviation of an operating limit parameter value, the date, time, and duration of the deviation, a brief explanation of the cause of the deviation and the corrective action taken, and whether the deviation occurred during a period of startup, shutdown, or malfunction.

(6) For each affected source, records of production rate on a process throughput basis (either feed rate to the process unit or discharge rate from the process unit).

(7) Records of any approved alternative monitoring method(s) or test procedure(s).

(8) Records of maintenance activities and inspections performed on control devices, including all records associated with the scheduled maintenance of continuous kiln control devices, as specified in § 63.9792(e).

(9) If you operate a source that is subject to the THC emission limits specified in item 2, 3, 6, or 7 of Table 1 to this subpart and is controlled with a catalytic oxidizer, records of annual checks of catalyst activity levels and subsequent corrective actions.

(10) Current copies of the SSMP and the OM&M plan, including any revisions and records documenting conformance with those revisions.

§ 63.9818 In what form and how long must I keep my records?

(a) Your records must be in a form suitable and readily available for expeditious review, according to § 63.10(b)(1).

(b) As specified in § 63.10(b)(1), you must keep each record for 5 years following the date of each occurrence, measurement, maintenance, corrective action, report, or record.

(c) You must keep each record onsite for at least 2 years after the date of each occurrence, measurement, maintenance, corrective action, report, or record, according to § 63.10(b)(1). You may keep the records offsite for the remaining 3 years.

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OTHER REQUIREMENTS AND INFORMATION

§ 63.9820 What parts of the General Provisions apply to me?

Table 11 to this subpart shows which parts of the General Provisions specified in §§63.1 through 63.15 apply to you.

§ 63.9822 Who implements and enforces this subpart?

(a) This subpart can be implemented and enforced by us, the U.S. Environmental Protection Agency (U.S. EPA), or a delegated authority such as your State, local, or tribal agency. If the U.S. EPA Administrator has delegated authority to your State, local, or tribal agency, then that agency, in addition to the U.S. EPA, has the authority to implement and enforce this subpart. You should contact your U.S. EPA Regional Office to find out if implementation and enforcement to this subpart is delegated to your State, local, or tribal agency.

(b) In delegating implementation and enforcement authority to this subpart to a State, local, or tribal agency under 40 CFR part 63, subpart E, the authorities contained in paragraph (c) of this section are retained by the Administrator of the U.S. EPA and are not transferred to the State, local, or tribal agency.

(c) The authorities that cannot be delegated to State, local, or tribal agencies are as specified in paragraphs (c)(1) through (4) of this section.

(1) Approval of alternatives to the applicability requirements in §§63.9782 and 63.9784, the compliance date requirements in §63.9786, and the emission limitations in §63.9788.

(2) Approval of major changes to test methods under §63.7(e)(2)(ii) and (f) and as defined in §63.90.

(3) Approval of major changes to monitoring under §63.8(f) and as defined in §63.90.

(4) Approval of major changes to recordkeeping and reporting under §63.10(f) and as defined in §63.90.

§ 63.9824 What definitions apply to this subpart?

Terms used in this subpart are defined in the Clean Air Act, in 40 CFR

63.2, the General Provisions of this part, and in this section as follows:

Additive means a minor addition of a chemical, mineral, or metallic substance that is added to a refractory mixture to facilitate processing or impart specific properties to the final refractory product.

Add-on air pollution control device (APCD) means equipment installed on a process vent that reduces the quantity of a pollutant that is emitted to the air.

Autoclave means a vessel that is used to impregnate fired and/or unfired refractory shapes with pitch to form pitch-impregnated refractory products. Autoclaves also can be used as defumers following the impregnation process.

Bag leak detection system means an instrument that is capable of monitoring particulate matter loadings in the exhaust of a fabric filter in order to detect bag failures. A bag leak detection system includes, but is not limited to, an instrument that operates on triboelectric, light-scattering, light-transmittance, or other effects to monitor relative PM loadings.

Basket means the metal container used to hold refractory shapes for pitch impregnation during the shape preheating, impregnation, defuming, and, if applicable, coking processes.

Batch process means a process in which a set of refractory shapes is acted upon as a single unit according to a predetermined schedule, during which none of the refractory shapes being processed are added or removed. A batch process does not operate continuously.

Binder means a substance added to a granular material to give it workability and green or dry strength.

Catalytic oxidizer means an add-on air pollution control device that is designed specifically to destroy organic compounds in a process exhaust gas stream by catalytic incineration. A catalytic oxidizer includes a bed of catalyst media through which the process exhaust stream passes to promote combustion and incineration at a lower temperature than would be possible without the catalyst.

Chromium refractory product means a refractory product that contains at least 1 percent chromium by weight.

Clay refractory product means a refractory product that contains at least 10 percent uncalcined clay by weight prior to firing in a kiln. In this definition, the term "clay" means any of the following six classifications of clay defined by the U.S. Geologic Survey: ball clay, bentonite, common clay and shale, fire clay, fuller's earth, and kaolin.

Coking oven means a thermal process unit that operates at a peak temperature typically between 540° and 870 °C (1000° and 1600 °F) and is used to drive off the volatile constituents of pitch-impregnated refractory shapes under a reducing or oxygen-deprived atmosphere.

Continuous parameter monitoring system (CPMS) means the total equipment that is used to measure and record temperature, pressure, liquid flow rate, gas flow rate, or pH on a continuous basis in one or more locations. "Total equipment" includes the sensor, mechanical components, electronic components, data acquisition system, data recording system, electrical wiring, and other components of a CPMS.

Continuous process means a process that operates continuously. In a continuous process unit, the materials or shapes that are processed are either continuously charged (fed) to and discharged from the process unit, or are charged and discharged at regular time intervals without the process unit being shut down. Continuous thermal process units, such as tunnel kilns, generally include temperature zones that are maintained at relatively constant temperature and through which the materials or shapes being processed are conveyed continuously or at regular time intervals.

Curing oven means a thermal process unit that operates at a peak temperature typically between 90° and 340 °C (200° and 650 °F) and is used to activate a thermosetting resin, pitch, or other binder in refractory shapes. Curing ovens also perform the same function as shape dryers in removing the free moisture from refractory shapes.

Defumer means a process unit that is used for holding pitch-impregnated re-

fractory shapes as the shapes defume or cool immediately following the impregnation process. This definition includes autoclaves that are opened and exhausted to the atmosphere following an impregnation cycle and used for holding pitch-impregnated refractory shapes while the shapes defume or cool.

Deviation means any instance in which an affected source subject to this subpart, or an owner or operator of such a source:

(1) Fails to meet any requirement or obligation established by this subpart including, but not limited to, any emission limitation (emission limit, operating limit, or work practice standard);

(2) Fails to meet any term or condition that is adopted to implement an applicable requirement in this subpart for any affected source required to obtain such a permit; or

(3) Fails to meet any emission limitation (emission limit, operating limit, or work practice standard) in this subpart during startup, shutdown, or malfunction, regardless of whether or not such failure is permitted by this subpart.

Dry injection fabric filter (DIFF) means an add-on air pollution control device that includes continuous injection of hydrated lime or other sorbent into a duct or reaction chamber followed by a fabric filter.

Dry lime scrubber/fabric filter (DLS/FF) means an add-on air pollution control device that includes continuous injection of humidified hydrated lime or other sorbent into a reaction chamber followed by a fabric filter. These systems may include recirculation of some of the sorbent.

Dry limestone adsorber (DLA) means an air pollution control device that includes a limestone storage bin, a reaction chamber that is essentially a packed-tower filled with limestone, and may or may not include a peeling drum that mechanically scrapes reacted limestone to regenerate the stone for reuse.

Emission limitation means any restriction on the emissions a process unit may discharge.

Fabric filter means an add-on air pollution control device used to capture particulate matter by filtering a process exhaust stream through a filter or

filter media; a fabric filter is also known as a baghouse.

Fired refractory shape means a refractory shape that has been fired in a kiln.

HAP means any hazardous air pollutant that appears in section 112(b) of the Clean Air Act.

Kiln means a thermal process unit that operates at a peak temperature greater than 820 °C (1500 °F) and is used for firing or sintering refractory, ceramic, or other shapes.

Kiln furniture means any refractory shape that is used to hold, support, or position ceramic or refractory products in a kiln during the firing process.

Maximum organic HAP processing rate means the combination of process and refractory product formulation that has the greatest potential to emit organic HAP. The maximum organic HAP processing rate is a function of the organic HAP processing rate, process operating temperature, and other process operating parameters that affect emissions of organic HAP. (See also the definition of *organic HAP processing rate*.)

Organic HAP processing rate means the rate at which the mass of organic HAP materials contained in refractory shapes are processed in an affected thermal process unit. The organic HAP processing rate is a function of the amount of organic HAP contained in the resins, binders, and additives used in a refractory mix; the amounts of those resins, binders, and additives in the refractory mix; and the rate at which the refractory shapes formed from the refractory mix are processed in an affected thermal process unit. For continuous process units, the organic HAP processing rate is expressed in units of mass of organic HAP per unit of time (e.g., pounds per hour). For batch process units, the organic HAP processing rate is expressed in units of mass of organic HAP per unit mass of refractory shapes processed during the batch process cycle (e.g., pounds per ton).

Particulate matter (PM) means, for the purposes of this subpart, emissions of particulate matter that serve as a measure of total particulate emissions as measured by EPA Method 5 of 40 CFR part 60, appendix A.

Peak emissions period means the period of consecutive hourly mass emissions of the applicable pollutant that is greater than any other period of consecutive hourly mass emissions for the same pollutant over the course of a specified batch process cycle, as defined in paragraphs (1) and (2) of this definition. The peak emissions period is a function of the rate at which the temperature of the refractory shapes is increased, the mass and loading configuration of the shapes in the process unit, the constituents of the refractory mix, and the type of pollutants emitted.

(1) The 3-hour peak THC emissions period is the period of 3 consecutive hours over which the sum of the hourly THC mass emissions rates is greater than the sum of the hourly THC mass emissions rates for any other period of 3 consecutive hours during the same batch process cycle.

(2) The 3-hour peak HF emissions period is the period of 3 consecutive hours over which the sum of the hourly HF mass emissions rates is greater than the sum of the hourly HF mass emissions rates for any other period of 3 consecutive hours during the same batch process cycle.

Period of natural gas curtailment or supply interruption means a period of time during which the supply of natural gas to an affected facility is halted for reasons beyond the control of the facility. An increase in the cost or unit price of natural gas does not constitute a period of natural gas curtailment or supply interruption.

Pitch means the residue from the distillation of petroleum or coal tar.

Pitch-bonded refractory product means a formed refractory product that is manufactured using pitch as a bonding agent. Pitch-bonded refractory products are manufactured by mixing pitch with magnesium oxide, graphite, alumina, silicon carbide, silica, or other refractory raw materials, and forming the mix into shapes. After forming, pitch-bonded refractory products are cured in a curing oven and may be subsequently fired in a kiln.

Pitch-impregnated refractory product means a refractory shape that has been fired in a kiln, then impregnated with heated coal tar or petroleum pitch

under pressure. After impregnation, pitch-impregnated refractory shapes may undergo the coking process in a coking oven. The total carbon content of a pitch-impregnated refractory product is less than 50 percent.

Pitch working tank means a tank that is used for heating pitch to the impregnation temperature, typically between 150° and 260 °C (300° and 500 °F); temporarily storing heated pitch between impregnation cycles; and transferring pitch to and from the autoclave during the impregnation step in manufacturing pitch-impregnated refractory products.

Plant site means all contiguous or adjoining property that is under common control, including properties that are separated only by a road or other public right-of-way. Common control includes properties that are owned, leased, or operated by the same entity, parent entity, subsidiary, or any combination thereof.

Redundant sensor means a second sensor or a back-up sensor that is integrated into a CPMS and is used to check the parameter value (e.g., temperature, pressure) measured by the primary sensor of the CPMS.

Refractory product means nonmetallic materials containing less than 50 percent carbon by weight and having those chemical and physical properties that make them applicable for structures, or as components of systems, that are exposed to environments above 538 °C (1000 °F). This definition includes, but is not limited to: refractory bricks, kiln furniture, crucibles, refractory ceramic fiber, and other materials used as linings for boilers, kilns, and other processing units and equipment where extremes of temperature, corrosion, and abrasion would destroy other materials.

Refractory products that use organic HAP means resin-bonded refractory products, pitch-bonded refractory products, and other refractory products that are produced using a substance that is an organic HAP, that releases an organic HAP during production of the refractory product, or that contains an organic HAP, such as methanol or ethylene glycol.

Refractory shape means any refractory piece forming a stable mass with specific dimensions.

Research and development process unit means any process unit whose purpose is to conduct research and development for new processes and products and is not engaged in the manufacture of products for commercial sale, except in a de minimis manner.

Resin-bonded refractory product means a formed refractory product that is manufactured using a phenolic resin or other type of thermosetting resin as a bonding agent. Resin-bonded refractory products are manufactured by mixing resin with alumina, magnesium oxide, graphite, silica, zirconia, or other refractory raw materials, and forming the mix into shapes. After forming, resin-bonded refractory products are cured in a curing oven and may be subsequently fired in a kiln.

Responsible official means one of the following:

(1) For a corporation: a president, secretary, treasurer, or vice-president of the corporation in charge of a principal business function, or any other person who performs similar policy or decisionmaking functions for the corporation, or a duly authorized representative of such person if the representative is responsible for the overall operation of one or more manufacturing, production, or operating facilities applying for or subject to a permit and either:

(i) The facilities employ more than 250 persons or have gross annual sales or expenditures exceeding \$25 million (in second quarter 1980 dollars); or

(ii) The delegation of authority to such representatives is approved in advance by the Administrator;

(2) For a partnership or sole proprietorship: a general partner or the proprietor, respectively;

(3) For a municipality, State, Federal, or other public agency: either a principal executive officer or ranking elected official. For the purposes of this part, a principal executive officer of a Federal agency includes the chief executive officer having responsibility for the overall operations of a principal geographic unit of the agency (e.g., a Regional Administrator of EPA); or

(4) For affected sources (as defined in this subpart) applying for or subject to a title V permit: "responsible official" shall have the same meaning as defined in part 70 or Federal title V regulations in this chapter (42 U.S.C. 7661), whichever is applicable.

Shape dryer means a thermal process unit that operates at a peak temperature typically between 40° and 700 °C (100° and 1300 °F) and is used exclusively to reduce the free moisture content of a refractory shape. Shape dryers generally are the initial thermal process step following the forming step in refractory products manufacturing. (See also the definition of a *curing oven*.)

Shape preheater means a thermal process unit that operates at a peak temperature typically between 180° and 320 °C (350° and 600 °F) and is used to heat fired refractory shapes prior to

the impregnation step in manufacturing pitch-impregnated refractory products.

Thermal oxidizer means an add-on air pollution control device that includes one or more combustion chambers and is designed specifically to destroy organic compounds in a process exhaust gas stream by incineration.

Uncalcined clay means clay that has not undergone thermal processing in a calciner.

Wet scrubber means an add-on air pollution control device that removes pollutants from a gas stream by bringing them into contact with a liquid, typically water.

Work practice standard means any design, equipment, work practice, or operational standard, or combination thereof, that is promulgated pursuant to section 112(h) of the Clean Air Act.

TABLE 1 TO SUBPART SSSSS OF PART 63—EMISSION LIMITS

As stated in §63.9788, you must comply with the emission limits for affected sources in the following table:

For	You must meet the following emission limits
1. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 2 through 9 of this table.
2. Continuous process units that are controlled with a thermal or catalytic oxidizer.	a. The 3-hour block average THC concentration must not exceed 20 parts per million by volume, dry basis (ppmvd), corrected to 18 percent oxygen, at the outlet of the control device; or
3. Continuous process units that are equipped with a control device other than a thermal or catalytic oxidizer.	b. The 3-hour block average THC mass emissions rate must be reduced by at least 95 percent.
4. Continuous process units that use process changes to reduce organic HAP emissions.	a. The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or
5. Continuous kilns that are not equipped with a control device	b. The 3-hour block average THC mass emissions rate must be reduced by at least 95 percent.
6. Batch process units that are controlled with a thermal or catalytic oxidizer.	The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
7. Batch process units that are equipped with a control device other than a thermal or catalytic oxidizer.	The 3-hour block average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
	a. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or
	b. The 2-run block average THC mass emissions rate for the 3-hour peak emissions period must be reduced by at least 95 percent.
	a. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the control device; or
	b. The 2-run block average THC mass emissions rate for the 3-hour peak emissions period must be reduced by at least 95 percent.

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For . . .	You must meet the following emission limits
8. Batch process units that use process changes to reduce organic HAP emissions.	b. The 2-run block average THC mass emissions rate for the 3-hour peak emissions period must be reduced by at least 95 percent. The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
9. Batch process kilns that are not equipped with a control device.	The 2-run block average THC concentration for the 3-hour peak emissions period must not exceed 20 ppmvd, corrected to 18 percent oxygen, at the outlet of the process gas stream.
10. Each new continuous kiln that is used to produce clay refractory products.	a. The 3-hour block average HF emissions must not exceed 0.019 kilograms per megagram (kg/Mg) (0.038 pounds per ton (lb/ton)) of uncalcined clay processed, OR the 3-hour block average HF mass emissions rate must be reduced by at least 90 percent; and b. The 3-hour block average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed, OR the 3-hour block average HCl mass emissions rate must be reduced by at least 30 percent.
11. Each new batch process kiln that is used to produce clay refractory products.	a. The 2-run block average HF mass emissions rate for the 3-hour peak emissions period must be reduced by at least 90 percent; and b. The 2-run block average HCl mass emissions rate for the 3-hour peak emissions period must be reduced by at least 30 percent.

TABLE 2 TO SUBPART SSSSS OF PART 63—OPERATING LIMITS

As stated in §63.9788, you must comply with the operating limits for affected sources in the following table:]

For . . .	You must
1. Each affected source listed in Table 1 to this subpart	a. Operate all affected sources according to the requirements to this subpart on and after the date on which the initial performance test is conducted or required to be conducted, whichever date is earlier; and b. Capture emissions and vent them through a closed system; and c. Operate each control device that is required to comply with this subpart on each affected source during all periods that the source is operating, except where specified in §63.9792(e), item 2 of this table, and item 13 of Table 4 to this subpart; and d. Record all operating parameters specified in Table 8 to this subpart for the affected source; and e. Prepare and implement a written OM&M plan as specified in §63.9792(d).
2. Each affected continuous kiln that is equipped with an emission control device.	a. Receive approval from the Administrator before taking the control device on the affected kiln out of service for scheduled maintenance, as specified in §63.9792(e); and b. Minimize HAP emissions from the affected kiln during all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service; and c. Minimize the duration of all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service.
3. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	Satisfy the applicable operating limits specified in items 4 through 9 of this table.
4. Each affected continuous process unit	Maintain the 3-hour block average organic HAP processing rate (pounds per hour) at or below the maximum organic HAP processing rate established during the most recent performance test.

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For . . .	You must . . .
5. Continuous process units that are equipped with a thermal oxidizer.	Maintain the 3-hour block average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature for the oxidizer established during the most recent performance test.
6. Continuous process units that are equipped with a catalytic oxidizer.	<ul style="list-style-type: none"> a. Maintain the 3-hour block average operating temperature at the inlet of the catalyst bed of the oxidizer at or above the minimum allowable operating temperature for the oxidizer established during the most recent performance test; and b. Check the activity level of the catalyst at least every 12 months.
7. Each affected batch process unit	For each batch cycle, maintain the organic HAP processing rate (pounds per batch) at or below the maximum organic HAP processing rate established during the most recent performance test.
8. Batch process units that are equipped with a thermal oxidizer.	<ul style="list-style-type: none"> a. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintain the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 11 of Table 4 to this subpart; and b. For each subsequent hour of the batch cycle, maintain the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart.
9. Batch process units that are equipped with a catalytic oxidizer.	<ul style="list-style-type: none"> a. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintain the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 12 of Table 4 to this subpart; and b. For each subsequent hour of the batch cycle, maintain the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and c. Check the activity level of the catalyst at least every 12 months.
10. Each new kiln that is used to process clay refractory products.	Satisfy the applicable operating limits specified in items 11 through 13 of this table.
11. Each affected kiln that is equipped with a DLA	<ul style="list-style-type: none"> a. Maintain the 3-hour block average pressure drop across the DLA at or above the minimum levels established during the most recent performance test; and b. Maintain free-flowing limestone in the feed hopper, silo, and DLA at all times; and c. Maintain the limestone feeder at or above the level established during the most recent performance test; and d. Use the same grade of limestone from the same source as was used during the most recent performance test and maintain records of the source and type of limestone used.
12. Each affected kiln that is equipped with a DIFF or DLS/FF	<ul style="list-style-type: none"> a. Initiate corrective action within 1 hour of a bag leak detection system alarm and complete corrective actions in accordance with the OM&M plan; and b. Verify at least once each 8-hour shift that lime is free-flowing by means of a visual check, checking the output of a load cell, carrier gas/lime flow indicator, or carrier gas pressure drop measurement system; and c. Record the lime feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test.
13. Each affected kiln that is equipped with a wet scrubber	<ul style="list-style-type: none"> a. Maintain the 3-hour block average pressure drop across the scrubber, liquid pH, and liquid flow rate at or above the minimum levels established during the most recent performance test; and b. If chemicals are added to the scrubber liquid, maintain the 3-hour block average chemical feed rate at or above the minimum chemical feed rate established during the most recent performance test.

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TABLE 3 TO SUBPART SSSSS OF PART 63—WORK PRACTICE STANDARDS

As stated in §63.9788, you must comply with the work practice standards for affected sources in the following table:

For . . .	You must . . .	According to one of the following requirements . . .
1. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	a. Control POM emissions from any affected shape preheater.	i. At least every 10 preheating cycles, clean the residual pitch from the surfaces of the basket or container by abrasive blasting prior to placing the basket or container in the affected shape preheater; or ii. At least every 10 preheating cycles, subject the basket or container to a thermal process cycle that meets or exceeds the operating temperature and cycle time of the affected preheater, AND is conducted in a process unit that is exhausted to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven; or iii. Capture emissions from the affected shape preheater and vent them to the control device that is used to control emissions from an affected defumer or coking oven, or to a comparable thermal or catalytic oxidizer.
2. Each new or existing pitch working tank.	Control POM emissions	Capture emissions from the affected pitch working tank and vent them to the control device that is used to control emissions from an affected defumer or coking oven, OR to a comparable thermal or catalytic oxidizer.
3. Each new or existing chromium refractory products kiln.	Minimize fuel-based HAP emissions	Use natural gas, or equivalent, as the kiln fuel, except during periods of natural gas curtailment or supply interruption, as defined in § 63.9824.
4. Each existing clay refractory products kiln.	Minimize fuel-based HAP emissions	Use natural gas, or equivalent, as the kiln fuel, except during periods of natural gas curtailment or supply interruption, as defined in § 63.9824.

TABLE 4 TO SUBPART SSSSS TO PART 63—REQUIREMENTS FOR PERFORMANCE TESTS

As stated in §63.9800, you must comply with the requirements for performance tests for affected sources in the following table:

For . . .	You must . . .	Using . . .	According to the following requirements . . .
1. Each affected source listed in Table 1 to this subpart.	a. Conduct performance tests	i. The requirements of the general provisions in subpart A of this part and the requirements to this subpart.	(1) Record the date of the test; and (2) Identify the emission source that is tested; and (3) Collect and record the corresponding operating parameter and emission test data listed in this table for each run of the performance test; and (4) Repeat the performance test at least every 5 years; and (5) Repeat the performance test before changing the parameter value for any operating limit specified in your OM&M plan; and

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
	<p>b. Select the locations of sampling ports and the number of traverse points.</p>	<p>i. Method 1 or 1A of 40 CFR part 60, appendix A.</p>	<p>(6) If complying with the THC concentration or THC percentage reduction limits specified in items 2 through 9 of Table 1 to this subpart, repeat the performance test under the conditions specified in items 2.a.2. and 2.a.3. of this table; and</p> <p>(7) If complying with the emission limits for new clay refractory products kilns specified in items 10 and 11 of Table 1 to this subpart, repeat the performance test under the conditions specified in items 14.a.1.4. and 17.a.1.4. of this table.</p>
	<p>c. Determine gas velocity and volumetric flow rate.</p>	<p>Method 2, 2A, 2C, 2D, 2F, or 2G of 40 CFR part 60, appendix A.</p>	<p>(1) To demonstrate compliance with the percentage reduction limits specified in items 2.b., 3.b., 6.b., 7.b., 10, and 11 of Table 1 to this subpart, locate sampling sites at the inlet of the control device and at either the outlet of the control device or at the stack prior to any releases to the atmosphere; and</p> <p>(2) To demonstrate compliance with any other emission limit specified in Table 1 to this subpart, locate all sampling sites at the outlet of the control device or at the stack prior to any releases to the atmosphere.</p>
	<p>d. Conduct gas molecular weight analysis.</p>	<p>(i) Method 3, 3A, or 3B of 40 CFR part 60, appendix A; or</p> <p>(ii) ASME PTC 19.10-1981-Part 10.</p>	<p>Measure gas velocities and volumetric flow rates at 1-hour intervals throughout each test run.</p> <p>As specified in the applicable test method.</p> <p>You may use ASME PTC 19.10-1981-Part 10 (available for purchase from Three Park Avenue, New York, NY 10016-5990) as an alternative to EPA Method 3B.</p>
	<p>e. Measure gas moisture content</p>	<p>Method 4 of 40 CFR part 60, appendix A.</p>	<p>As specified in the applicable test method.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.</p>	<p>a. Conduct performance tests</p> <p>b. Satisfy the applicable requirements listed in items 3 through 13 of this table.</p>	<p>.....</p>	<p>(1) Conduct the performance test while the source is operating at the maximum organic HAP processing rate, as defined in § 63.9824, reasonably expected to occur; and</p> <p>(2) Repeat the performance test before starting production of any product for which the organic HAP processing rate is likely to exceed the maximum organic HAP processing rate established during the most recent performance test by more than 10 percent, as specified in § 63.9798(c); and</p> <p>(3) Repeat the performance test on any affected uncontrolled kiln following process changes (e.g., shorter curing oven cycle time) that could increase organic HAP emissions from the affected kiln, as specified in § 63.9798(d).</p>
<p>3. Each affected continuous process unit.</p>	<p>a. Perform a minimum of 3 test runs.</p> <p>b. Establish the operating limit for the maximum organic HAP processing rate.</p> <p>c. Record the operating temperature of the affected source.</p>	<p>The appropriate test methods specified in items 1, 4, and 5 of this table.</p> <p>i. Method 311 of 40 CFR part 63, appendix A, OR material safety data sheets (MSDS), OR product labels to determine the mass fraction of organic HAP in each resin, binder, or additive; and</p> <p>ii. Product formulation data that specify the mass fraction of each resin, binder, and additive in the products that are processed during the performance test; and</p> <p>iii. Process feed rate data (tons per hour).</p> <p>Process data</p>	<p>Each test run must be at least 1 hour in duration.</p> <p>(1) Calculate and record the organic HAP content of all refractory shapes that are processed during the performance test, based on the mass fraction of organic HAP in the resins, binders, or additives; the mass fraction of each resin, binder, or additive, in the product; and the process feed rate; and</p> <p>(2) Calculate and record the organic HAP processing rate (pounds per hour) for each test run; and</p> <p>(3) Calculate and record the maximum organic HAP processing rate as the average of the organic HAP processing rates for the three test runs.</p> <p>During each test run and at least once per hour, record the operating temperature in the highest temperature zone of the affected source.</p>

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
4. Each contin-uous process unit that is sub-ject to the THC emission limit listed in item 2.a., 3.a., 4, or 5 of Table 1 to this subpart.	a. Measure THC concentrations at the outlet of the control device or in the stack.	i. Method 25A of 40 CFR part 60, appendix A.	(1) Each minute, measure and record the concentrations of THC in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentra-tion.
	b. Measure oxygen concentrations at the outlet of the control de-vice or in the stack.	i. Method 3A of 40 CFR part 60, appendix A.	(1) Each minute, measure and record the concentrations of ox-ygen in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentra-tion.
	c. Determine the hourly average THC concentration, corrected to 18 percent oxygen.	i. Equation 1 of §63.9800(g)(1), and. ii. The 1-minute THC and oxygen concentration data.	(1) Calculate the hourly average THC concentration for each hour of the performance test as the average of the 1-minute THC measurements; and (2) Calculate the hourly average oxygen concentration for each hour of the performance test as the average of the 1-minute ox-ygen measurements; and (3) Correct the hourly average THC concentrations to 18 per-cent oxygen using Equation 1 of §63.9800(g)(1).
	d. Determine the 3-hour block av-erage THC emission concentra-tion, corrected to 18 percent ox-ygen.	The hourly average concentration of THC, corrected to 18 percent oxygen, for each test run.	Calculate the 3-hour block av-erage THC emission concentra-tion, corrected to 18 percent ox-ygen, as the average of the hourly average THC emission concentrations, corrected to 18 percent oxygen.
5. Each contin-uous process unit that is sub-ject to the THC percentage re-duction limit listed in item 2.b. or 3.b. of Table 1 to this subpart.	a. Measure THC concentrations at the inlet and outlet of the con-trol device.	i. Method 25A of 40 CFR part 60, appendix A.	(1) Each minute, measure and record the concentrations of THC at the inlet and outlet of the control device; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentra-tion at the control device inlet and outlet.
	b. Determine the hourly THC mass emissions rates at the inlet and outlet of the control device.	i. The 1-minute THC concentration data at the control device inlet and outlet; and ii. The volumetric flow rates at the control device inlet and outlet.	Calculate the hourly THC mass emissions rates at the control device inlet and outlet for each hour of the performance test.
	c. Determine the 3-hour block av-erage THC percentage reduc-tion.	i. The hourly THC mass emissions rates at the inlet and outlet of the control device.	(1) Calculate the hourly THC per-centage reduction for each hour of the performance test using Equation 2 of §63.9800(g)(1); and (2) Calculate the 3-hour block av-erage THC percentage reduc-tion.

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
6. Each continuous process unit that is equipped with a thermal oxidizer.	a. Establish the operating limit for the minimum allowable thermal oxidizer combustion chamber temperature.	i. Continuous recording of the output of the combustion chamber temperature measurement device.	(1) At least every 15 minutes, measure and record the thermal oxidizer combustion chamber temperature; and (2) Provide at least one measurement during at least three 15-minute periods per hour of testing; and (3) Calculate the hourly average thermal oxidizer combustion chamber temperature for each hour of the performance test; and (4) Calculate the minimum allowable combustion chamber temperature as the average of the combustion chamber temperatures for the three test runs, minus 14 °C (25 °F).
7. Each continuous process unit that is equipped with a catalytic oxidizer.	a. Establish the operating limit for the minimum allowable temperature at the inlet of the catalyst bed.	i. Continuous recording of the output of the temperature measurement device.	(1) At least every 15 minutes, measure and record the temperature at the inlet of the catalyst bed; and (2) Provide at least one catalyst bed inlet temperature measurement during at least three 15-minute periods per hour of testing; and (3) Calculate the hourly average catalyst bed inlet temperature for each hour of the performance test; and (4) Calculate the minimum allowable catalyst bed inlet temperature as the average of the catalyst bed inlet temperatures for the three test runs, minus 14 °C (25 °F).
8. Each affected batch process unit.	a. Perform a minimum of two test runs.	i. The appropriate test methods specified in items 1, 9, and 10 of this table.	(1) Each test run must be conducted over a separate batch cycle unless you satisfy the requirements of § 63.9800(f)(3) and (4); and (2) Each test run must begin with the start of a batch cycle, except as specified in item 8.a.i.4. of this table; and (3) Each test run must continue until the end of the batch cycle, except as specified in items 8.a.i.4. and 8.a.i.5. of this table; and (4) If you develop an emissions profile, as described in § 63.9802(a), AND for sources equipped with a thermal or catalytic oxidizer, you do not reduce the oxidizer operating temperature, as specified in item 13 of this table, you can limit each test run to the 3-hour peak THC emissions period; and

For . . .	You must . . .	Using . . .	According to the following require-ments . . .
<p>9. Each batch process unit that is subject to the THC emission limit listed in item 6.a., 7.a., 8, or 9 of Table 1 to this subpart.</p>	<p>b. Establish the operating limit for the maximum organic HAP processing rate.</p> <p>c. Record the batch cycle time</p> <p>d. Record the operating temperature of the affected source.</p> <p>a. Measure THC concentrations at the outlet of the control device or in the stack.</p>	<p>i. Method 311 of 40 CFR part 63, appendix A, OR MSDS, OR product labels to determine the mass fraction of organic HAP in each resin, binder, or additive; and</p> <p>ii. Product formulation data that specify the mass fraction of each resin, binder, and additive in the products that are processed during the performance test; and</p> <p>iii. Batch weight (tons)</p> <p>Process data</p> <p>Process data</p> <p>i. Method 25A of 40 CFR part 60, appendix A.</p>	<p>(5) If you do not develop an emissions profile, a test run can be stopped, and the results of that run considered complete, if you measure emissions continuously until at least 3 hours after the affected process unit has reached maximum temperature, AND the hourly average THC mass emissions rate has not increased during the 3-hour period since maximum process temperature was reached, and the hourly average concentrations of THC at the inlet of the control device have not exceeded 20 ppmvd, corrected to 18 percent oxygen, during the 3-hour period since maximum process temperature was reached or the hourly average THC percentage reduction has been at least 95 percent during the 3-hour period since maximum process temperature was reached, AND, for sources equipped with a thermal or catalytic oxidizer, at least 1 hour has passed since any reduction in the operating temperature of the oxidizer, as specified in item 13 of this table.</p> <p>(1) Calculate and record the organic HAP content of all refractory shapes that are processed during the performance test, based on the mass fraction of HAP in the resins, binders, or additives; the mass fraction of each resin, binder, or additive, in the product, and the batch weight prior to processing; and</p> <p>(2) Calculate and record the organic HAP processing rate (pounds per batch) for each test run; and</p> <p>(3) Calculate and record the maximum organic HAP processing rate as the average of the organic HAP processing rates for the two test runs.</p> <p>Record the total elapsed time from the start to the completion of the batch cycle.</p> <p>Record the operating temperature of the affected source at least once every hour from the start to the completion of the batch cycle.</p> <p>(1) Each minute, measure and record the concentrations of THC in the exhaust stream; and</p> <p>(2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration.</p>

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
<p>10. Each batch process unit that is subject to the THC percentage reduction limit listed in item 6.b. or 7.b. of Table 1 to this subpart.</p>	<p>b. Measure oxygen concentrations at the outlet of the control device or in the stack.</p>	<p>i. Method 3A of 40 CFR part 60, appendix A.</p>	<p>(1) Each minute, measure and record the concentrations of oxygen in the exhaust stream; and (2) Provide at least 50 1-minute measurements for each valid hourly average oxygen concentration.</p>
	<p>c. Determine the hourly average THC concentration, corrected to 18 percent oxygen.</p>	<p>i. Equation 1 of §63.9800(g)(1); and ii. The 1-minute THC and oxygen concentration data.</p>	<p>(1) Calculate the hourly average THC concentration for each hour of the performance test as the average of the 1-minute THC measurements; and (2) Calculate the hourly average oxygen concentration for each hour of the performance test as the average of the 1-minute oxygen measurements; and (3) Correct the hourly average THC concentrations to 18 percent oxygen using Equation 1 of §63.9800(g)(1).</p>
	<p>d. Determine the 3-hour peak THC emissions period for each test run.</p>	<p>The hourly average THC concentrations, corrected to 18 percent oxygen.</p>	<p>Select the period of 3 consecutive hours over which the sum of the hourly average THC concentrations, corrected to 18 percent oxygen, is greater than the sum of the hourly average THC emission concentrations, corrected to 18 percent oxygen, for any other period of 3 consecutive hours during the test run.</p>
	<p>e. Determine the average THC concentration, corrected to 18 percent oxygen, for each test run.</p>	<p>The hourly average THC emission concentrations, corrected to 18 percent oxygen, for the 3-hour peak THC emissions period.</p>	<p>Calculate the average of the hourly average THC concentrations, corrected to 18 percent oxygen, for the 3 hours of the peak emissions period for each test run.</p>
<p>f. Determine the 2-run block average THC concentration, corrected to 18 percent oxygen, for the emission test.</p>	<p>The average THC concentration, corrected to 18 percent oxygen, for each test run.</p>	<p>Calculate the average of the average THC concentrations, corrected to 18 percent oxygen, for each run.</p>	
<p>a. Measure THC concentrations at the inlet and outlet of the control device.</p>	<p>i. Method 25A of 40 CFR part 60, appendix A.</p>	<p>(1) Each minute, measure and record the concentrations of THC at the control device inlet and outlet; and (2) Provide at least 50 1-minute measurements for each valid hourly average THC concentration at the control device inlet and outlet.</p>	
<p>b. Determine the hourly THC mass emissions rates at the control device inlet and outlet.</p>	<p>i. The 1-minute THC concentration data at the control device inlet and outlet; and ii. The volumetric flow rates at the control device inlet and outlet.</p>	<p>(1) Calculate the hourly mass emissions rates at the control device inlet and outlet for each hour of the performance test.</p>	
<p>c. Determine the 3-hour peak THC emissions period for each test run.</p>	<p>The hourly THC mass emissions rates at the control device inlet.</p>	<p>Select the period of 3 consecutive hours over which the sum of the hourly THC mass emissions rates at the control device inlet is greater than the sum of the hourly THC mass emissions rates at the control device inlet for any other period of 3 consecutive hours during the test run.</p>	
<p>d. Determine the average THC percentage reduction for each test run.</p>	<p>i. Equation 2 of §63.9800(g)(2); and ii. The hourly THC mass emissions rates at the control device inlet and outlet for the 3-hour peak THC emissions period.</p>	<p>Calculate the average THC percentage reduction for each test run using Equation 2 of §63.9800(g)(2).</p>	

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
11. Each batch process unit that is equipped with a thermal oxidizer.	<p>e. Determine the 2-run block average THC percentage reduction for the emission test.</p> <p>a. Establish the operating limit for the minimum thermal oxidizer combustion chamber temperature.</p>	<p>The average THC percentage reduction for each test run.</p> <p>i. Continuous recording of the output of the combustion chamber temperature measurement device.</p>	<p>Calculate the average of the average THC percentage reductions for each test run.</p> <p>(1) At least every 15 minutes, measure and record the thermal oxidizer combustion chamber temperature; and</p> <p>(2) Provide at least one temperature measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average combustion chamber temperature for each hour of the 3-hour peak emissions period, as defined in item 9.d. or 10.c. of this table, whichever applies; and</p> <p>(4) Calculate the minimum allowable thermal oxidizer combustion chamber operating temperature as the average of the hourly combustion chamber temperatures for the 3-hour peak emissions period, minus 14 °C (25 °F).</p>
12. Each batch process unit that is equipped with a catalytic oxidizer.	<p>a. Establish the operating limit for the minimum temperature at the inlet of the catalyst bed.</p>	<p>i. Continuous recording of the output of the temperature measurement device.</p>	<p>(1) At least every 15 minutes, measure and record the temperature at the inlet of the catalyst bed; and</p> <p>(2) Provide at least one catalyst bed inlet temperature measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average catalyst bed inlet temperature for each hour of the 3-hour peak emissions period, as defined in item 9.d. or 10.c. of this table, whichever applies; and</p> <p>(4) Calculate the minimum allowable catalytic oxidizer catalyst bed inlet temperature as the average of the hourly catalyst bed inlet temperatures for the 3-hour peak emissions period, minus 14 °C (25 °F).</p>
13. Each batch process unit that is equipped with a thermal or catalytic oxidizer.	<p>a. During each test run, maintain the applicable operating temperature of the oxidizer until emission levels allow the oxidizer to be shut off or the operating temperature of the oxidizer to be reduced.</p>		<p>(1) The oxidizer can be shut off or the oxidizer operating temperature can be reduced if you do not use an emission profile to limit testing to the 3-hour peak emissions period, as specified in item 8.a.i.4. of this table; and</p> <p>(2) At least 3 hours have passed since the affected process unit reached maximum temperature; and</p> <p>(3) The applicable emission limit specified in item 6.a. or 6.b. of Table 1 to this subpart was met during each of the previous three 1-hour periods; and</p> <p>(4) The hourly average THC mass emissions rate did not increase during the 3-hour period since maximum process temperature was reached; and</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>14. Each new continuous kiln that is used to process clay refractory products.</p>	<p>a. Measure emissions of HF and HCl.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or ii. Method 26 of 40 CFR part 60, appendix A; or iii. Method 320 of 40 CFR part 63, appendix A.</p>	<p>(5) The applicable emission limit specified in item 6.a. and 6.b. of Table 1 to this subpart was met during each of the four 15-minute periods immediately following the oxidizer temperature reduction; and (6) If the applicable emission limit specified in item 6.a. or 6.b. of Table 1 to this subpart was not met during any of the four 15-minute periods immediately following the oxidizer temperature reduction, you must return the oxidizer to its normal operating temperature as soon as possible and maintain that temperature for at least 1 hour; and (7) Continue the test run until the applicable emission limit specified in items 6.a. and 6.b. of Table 1 to this subpart is met for at least four consecutive 15-minute periods that immediately follow the temperature reduction; and (8) Calculate the hourly average oxidizer operating temperature for each hour of the performance test since the affected process unit reached maximum temperature. (1) Conduct the test while the kiln is operating at the maximum production level; and (2) You may use Method 26 of 40 CFR part 60, appendix A, only if no acid PM (e.g., HF or HCl dissolved in water droplets emitted by sources controlled by a wet scrubber) is present; and (3) If you use Method 320 of 40 CFR part 63, appendix A, you must follow the analyte spiking procedures of Section 13 of Method 320 unless you can demonstrate that the complete spiking procedure has been conducted at a similar source; and (4) Repeat the performance test if the affected source is controlled with a DLA and you change the source of the limestone used in the DLA. Each test run must be at least 1 hour in duration.</p>
<p>15. Each new continuous kiln that is subject to the production-based HF and HCl emission limits specified in items 10.a. and 10.b. of Table 1 to this subpart.</p>	<p>b. Perform a minimum of 3 test runs. a. Record the uncalcined clay processing rate.</p>	<p>The appropriate test methods specified in items 1 and 14.a. of this table. i. Production data; and ii. Product formulation data that specify the mass fraction of uncalcined clay in the products that are processed during the performance test.</p>	<p>(1) Record the production rate (tons per hour of fired product); and (2) Calculate and record the average rate at which uncalcined clay is processed (tons per hour) for each test run; and (3) Calculate and record the 3-run average uncalcined clay processing rate as the average of the average uncalcined clay processing rates for each test run.</p>

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For . . .	You must . . .	Using . . .	According to the following require-ments . . .
	b. Determine the HF mass emis-sions rate at the outlet of the control device or in the stack.	i. Method 26A of 40 CFR part 60, appendix A; or ii. Method 26 of 40 CFR part 60, appendix A; or iii. Method 320 of 40 CFR part 63, appendix A.	Calculate the HF mass emissions rate for each test.
	c. Determine the 3-hour block average production-based HF emissions rate.	i. The HF mass emissions rate for each test run; and ii. The average uncalcined clay processing rate.	(1) Calculate the hourly produc-tion-based HF emissions rate for each test run using Equation 3 of § 63.9800(g)(3); and (2) Calculate the 3-hour block average production-based HF emissions rate as the average of the hourly production-based HF emissions rates for each test run.
	d. Determine the HCl mass emis-sions rate at the outlet of the control device or in the stack.	i. Method 26A of 40 CFR part 60, appendix A; or ii. Method 26 of 40 CFR part 60, appendix A; or iii. Method 320 of 40 CFR part 63, appendix A.	Calculate the HCl mass emissions rate for each test run.
	e. Determine the 3-hour block average production-based HCl emissions rate.	i. The HCl mass emissions rate for each test run; and ii. The average uncalcined clay processing rate.	(1) Calculate the hourly produc-tion-based HCl emissions rate for each test run using Equation 3 of § 63.9800(g)(3); and (2) Calculate the 3-hour block average production-based HCl emissions rate as the average of the production-based HCl emissions rates for each test run.
	16. Each new continuous kiln that is subject to the HF and HCl percentage reduction limits specified in items 10.a. and 10.b. of Table 1 to this subpart.	a. Measure the HF mass emis-sions rates at the inlet and out-let of the control device.	i. Method 26A of 40 CFR part 60, appendix A; or ii. Method 26 of 40 CFR part 60, appendix A; or iii. Method 320 of 40 CFR part 63, appendix A.
b. Determine the 3-hour block average HF percentage reduction.		i. The HF mass emissions rates at the inlet and outlet of the control device for each test run	(1) Calculate the hourly HF per-centage reduction using Equa-tion 2 of § 63.9800(g)(2); and (2) Calculate the 3-hour block average HF percentage reduction as the average of the HF per-centage reductions for each test run.
c. Measure the HCl mass emis-sions rates at the inlet and out-let of the control device.		i. Method 26A of 40 CFR part 60, appendix A; or ii. Method 26 of 40 CFR part 60, appendix A; or iii. Method 320 of 40 CFR part 63, appendix A.	Calculate the HCl mass emissions rates at the control device inlet and outlet for each test run.
d. Determine the 3-hour block average HCl percentage reduc-tion.		i. The HCl mass emissions rates at the inlet and outlet of the control device for each test run.	(1) Calculate the hourly HCl per-centage reduction using Equa-tion 2 of § 63.9800(g)(2); and (2) Calculate the 3-hour block average HCl percentage reduction as the average of HCl percent-age reductions for each test run.

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>17. Each new batch process kiln that is used to process clay refractory products.</p>	<p>a. Measure emissions of HF and HCl at the inlet and outlet of the control device.</p> <p>b. Perform a minimum of 2 test runs.</p> <p>c. Determine the hourly HF and HCl mass emissions rates at the inlet and outlet of the control device.</p> <p>d. Determine the 3-hour peak HF emissions period.</p> <p>e. Determine the 2-run block average HF percentage reduction for the emissions test.</p>	<p>i. Method 26A of 40 CFR part 60, appendix A; or</p> <p>ii. Method 26 of 40 CFR part 60, appendix A; or</p> <p>iii. Method 320 of 40 CFR part 63, appendix A.</p> <p>i. The appropriate test methods specified in items 1 and 17.a. of this table.</p> <p>i. The appropriate test methods specified in items 1 and 17.a. of this table.</p> <p>The hourly HF mass emissions rates at the inlet of the control device.</p> <p>i. The hourly average HF emissions rates at the inlet and outlet of the control device.</p>	<p>(1) Conduct the test while the kiln is operating at the maximum production level; and</p> <p>(2) You may use Method 26 of 40 CFR part 60, appendix A, only if no acid PM (e.g., HF or HCl dissolved in water droplets emitted by sources controlled by a wet scrubber) is present; and</p> <p>(3) If you use Method 320 of 40 CFR part 63, you must follow the analyte spiking procedures of Section 13 of Method 320 unless you can demonstrate that the complete spiking procedure has been conducted at a similar source; and</p> <p>(4) Repeat the performance test if the affected source is controlled with a DLA and you change the source of the limestone used in the DLA.</p> <p>(1) Each test run must be conducted over a separate batch cycle unless you satisfy the requirements of § 63.9800(f)(3) and (4); and</p> <p>(2) Each test run must consist of a series of 1-hour runs at the inlet and outlet of the control device, beginning with the start of a batch cycle, except as specified in item 17.b.i.4. of this table; and</p> <p>(3) Each test run must continue until the end of the batch cycle, except as specified in item 17.b.i.4. of this table; and</p> <p>(4) If you develop an emissions profile, as described in § 63.9802(b), you can limit each test run to the 3-hour peak HF emissions period.</p> <p>Determine the hourly mass HF and HCl emissions rates at the inlet and outlet of the control device for each hour of each test run.</p> <p>Select the period of 3 consecutive hours over which the sum of the hourly HF mass emissions rates at the control device inlet is greater than the sum of the hourly HF mass emissions rates at the control device inlet for any other period of 3 consecutive hours during the test run.</p> <p>(1) Calculate the HF percentage reduction for each hour of the 3-hour peak HF emissions period using Equation 2 of § 63.9800(g)(2); and</p> <p>(2) Calculate the average HF percentage reduction for each test run as the average of the hourly HF percentage reductions for the 3-hour peak HF emissions period for that run; and</p>

For . . .	You must . . .	Using . . .	According to the following requirements . . .
18. Each new kiln that is used to process clay refractory products and is equipped with a DLA.	<p>f. Determine the 2-run block average HCl percentage reduction for the emission test.</p> <p>a. Establish the operating limit for the minimum pressure drop across the DLA.</p> <p>b. Establish the operating limit for the limestone feeder setting.</p>	<p>i. The hourly average HCl emissions rates at the inlet and outlet of the control device.</p> <p>Data from the pressure drop measurement device during the performance test.</p> <p>Data from the limestone feeder during the performance test.</p>	<p>(3) Calculate the 2-run block average HF percentage reduction for the emission test as the average of the average HF percentage reductions for the two test runs.</p> <p>(1) Calculate the HCl percentage reduction for each hour of the 3-hour peak HF emissions period using Equation 2 § 63.9800(g)(2); and</p> <p>(2) Calculate the average HCl percentage reduction for each test run as the average of the hourly HCl percentage reductions for the 3-hour peak HF emissions period for that run; and</p> <p>(3) Calculate the 2-run block average HCl percentage reduction for the emission test as the average of the average HCl percentage reductions for the two test runs.</p> <p>(1) At least every 15 minutes, measure the pressure drop across the DLA; and</p> <p>(2) Provide at least one pressure drop measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average pressure drop across the DLA for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum pressure drop as the average of the hourly average pressure drops across the DLA for the two or three test runs, whichever applies.</p> <p>(1) Ensure that limestone in the feed hopper, silo, and DLA is free-flowing at all times during the performance test; and</p> <p>(2) Establish the limestone feeder setting 1 week prior to the performance test; and</p> <p>(3) Record and maintain the feeder setting for the 1-week period that precedes the performance test and during the performance test.</p>
19. Each new kiln that is used to process clay refractory products and is equipped with a DIFF or DLS/FF.	<p>a. Document conformance with specifications and requirements of the bag leak detection system.</p> <p>b. Establish the operating limit for the lime feeder setting.</p>	<p>Data from the installation and calibration of the bag leak detection system.</p> <p>i. Data from the lime feeder during the performance test.</p>	<p>Submit analyses and supporting documentation demonstrating conformance with EPA guidance and specifications for bag leak detection systems as part of the Notification of Compliance Status.</p> <p>(1) For continuous lime injection systems, ensure that lime in the feed hopper or silo is free-flowing at all times during the performance test; and</p> <p>(2) Record the feeder setting for the three test runs; and</p> <p>(3) If the feed rate setting varies during the three test runs, calculate and record the average feed rate for the two or three test runs, whichever applies.</p>

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For . . .	You must . . .	Using . . .	According to the following requirements . . .
<p>20. Each new kiln that is used to process clay refractory products and is equipped with a wet scrubber.</p>	<p>a. Establish the operating limit for the minimum scrubber pressure drop.</p> <p>b. Establish the operating limit for the minimum scrubber liquid pH.</p> <p>c. Establish the operating limit for the minimum scrubber liquid flow rate.</p> <p>d. If chemicals are added to the scrubber liquid, establish the operating limit for the minimum scrubber chemical feed rate.</p>	<p>i. Data from the pressure drop measurement device during the performance test.</p> <p>i. Data from the pH measurement device during the performance test.</p> <p>i. Data from the flow rate measurement device during the performance test.</p> <p>i. Data from the chemical feed rate measurement device during the performance test.</p>	<p>(1) At least every 15 minutes, measure the pressure drop across the scrubber; and</p> <p>(2) Provide at least one pressure drop measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average pressure drop across the scrubber for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum pressure drop as the average of the hourly average pressure drops across the scrubber for the two or three test runs, whichever applies.</p> <p>(1) At least every 15 minutes, measure scrubber liquid pH; and</p> <p>(2) Provide at least one pH measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average pH values for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum liquid pH as the average of the hourly average pH measurements for the two or three test runs, whichever applies.</p> <p>(1) At least every 15 minutes, measure the scrubber liquid flow rate; and</p> <p>(2) Provide at least one flow rate measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average liquid flow rate for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum liquid flow rate as the average of the hourly average liquid flow rates for the two or three test runs, whichever applies.</p> <p>(1) At least every 15 minutes, measure the scrubber chemical feed rate; and</p> <p>(2) Provide at least one chemical feed rate measurement during at least three 15-minute periods per hour of testing; and</p> <p>(3) Calculate the hourly average chemical feed rate for each hour of the performance test; and</p> <p>(4) Calculate and record the minimum chemical feed rate as the average of the hourly average chemical feed rates for the two or three test runs, whichever applies.</p>

TABLE 5 TO SUBPART SSSSS OF PART 63—INITIAL COMPLIANCE WITH EMISSION LIMITS

As stated in §63.9806, you must show initial compliance with the emission limits for affected sources according to the following table:

For . . .	For the following emission limit . . .	You have demonstrated compliance if . . .
1. Each affected source listed in Table 1 to this subpart.	a. Each applicable emission limit listed in Table 1 to this subpart.	i. Emissions measured using the test methods specified in Table 4 to this subpart satisfy the applicable emission limits specified in Table 1 to this subpart; and ii. You establish and have a record of the operating limits listed in Table 2 to this subpart over the performance test period; and iii. You report the results of the performance test in the Notification of Compliance Status, as specified by § 63.9812(e)(1) and (2).
2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 3 through 8 of this table.	You have satisfied the applicable requirements specified in items 3 through 8 of this table.
3. Each affected continuous process unit that is subject to the THC emission concentration limit listed in item 2.a., 3.a., 4, or 5 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	The 3-hour block average THC emission concentration measured during the performance test using Methods 25A and 3A is equal to or less than 20 ppmvd, corrected to 18 percent oxygen.
4. Each affected continuous process unit that is subject to the THC percentage reduction limit listed in item 2.b. or 3.b. of Table 1 to this subpart.	The average THC percentage reduction must equal or exceed 95 percent.	The 3-hour block average THC percentage reduction measured during the performance test using Method 25A is equal to or greater than 95 percent.
5. Each affected batch process unit that is subject to the THC emission concentration limit listed in item 6.a., 7.a., 8, or 9 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	The 2-run block average THC emission concentration for the 3-hour peak emissions period measured during the performance test using Methods 25A and 3A is equal to or less than 20 ppmvd, corrected to 18 percent oxygen.
6. Each affected batch process unit that is subject to the THC percentage reduction limit listed in item 6.b. or 7.b. of Table 1 to this subpart.	The average THC percentage reduction must equal or exceed 95 percent.	The 2-run block average THC percentage reduction for the 3-hour peak emissions period measured during the performance test using Method 25A is equal to or exceeds 95 percent.
7. Each affected continuous or batch process unit that is equipped with a control device other than a thermal or catalytic oxidizer and is subject to the emission limit listed in item 3 or 7 of Table 1 to this subpart.	a. The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; or b. The average THC percentage reduction must equal or exceed 95 percent.	i. You have installed a THC CEMS at the outlet of the control device or in the stack of the affected source; and ii. You have satisfied the requirements of PS-8 of 40 CFR part 60, appendix B.
8. Each affected continuous or batch process unit that uses process changes to reduce organic HAP emissions and is subject to the emission limit listed in item 4 or 8 of Table 1 to this subpart.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	i. You have installed a THC CEMS at the outlet of the control device or in the stack of the affected source; and ii. You have satisfied the requirements of PS-8 of 40 CFR part 60, appendix B.
9. Each new continuous kiln that is used to process clay refractory products.	a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent.	i. The 3-hour block average production-based HF emissions rate measured during the performance test using one of the methods specified in item 14.a.i. of Table 4 to this subpart is equal to or less than 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; or ii. The 3-hour block average HF emissions reduction measured during the performance test is equal to or greater than 90 percent.

For . . .	For the following emission limit . . .	You have demonstrated compliance if . . .
10. Each new batch process kiln that is used to process clay refractory products.	<p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p> <p>a. The average uncontrolled HF emissions must be reduced by at least 90 percent.</p> <p>b. The average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. The 3-hour block average production-based HCl emissions rate measured during the performance test using one of the methods specified in item 14.a.i. of Table 4 to this subpart is equal to or less than 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; or</p> <p>ii. The 3-hour block average HCl emissions reduction measured during the performance test is equal to or greater than 30 percent.</p> <p>The 2-run block average HF emission reduction measured during the performance test is equal to or greater than 90 percent.</p> <p>The 2-run block average HCl emissions reduction measured during the performance test is equal to or greater than 30 percent.</p>

TABLE 6 TO SUBPART SSSSS OF PART 63—INITIAL COMPLIANCE WITH WORK PRACTICE STANDARDS

As stated in §63.9806, you must show initial compliance with the work practice standards for affected sources according to the following table:

For each . . .	For the following standard . . .	You have demonstrated initial compliance if . . .
1. Each affected source listed in Table 3 to this subpart.	a. Each applicable work practice standard listed in Table 3 to this subpart.	<p>i. You have selected a method for performing each of the applicable work practice standards listed in Table 3 to this subpart; and</p> <p>ii. You have included in your Initial Notification a description of the method selected for complying with each applicable work practice standard, as required by §63.9(b); and</p> <p>iii. You submit a signed statement with the Notification of Compliance Status that you have implemented the applicable work practice standard listed in Table 3 to this subpart; and</p> <p>iv. You have described in your OM&M plan the method for complying with each applicable work practice standard specified in Table 3 to this subpart.</p>
2. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	a. Control POM emissions from any affected shape preheater.	<p>i. You have implemented at least one of the work practice standards listed in item 1 of Table 3 to this subpart; and</p> <p>ii. You have established a system for recording the date and cleaning method for each time you clean an affected basket or container.</p>
3. Each affected new or existing pitch working tank.	Control POM emissions	You have captured and vented emissions from the affected pitch working tank to the device that is used to control emissions from an affected defumer or coking oven, or to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven.
4. Each new or existing chromium refractory products kiln.	Minimize fuel-basec HAP emissions	You use natural gas, or equivalent, as the kiln fuel.
5. Each existing clay refractory products kiln.	Minimize fuel-basec HAP emissions	You use natural gas, or equivalent, as the kiln fuel.

TABLE 7 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH EMISSION LIMITS

As stated in §63.9810, you must show continuous compliance with the emission limits for affected sources according to the following table:

For . . .	For the following emission limit . . .	You must demonstrate continuous compliance by . . .
1. Each affected source listed in Table 1 to this subpart.	a. Each applicable emission limit listed in Table 1 to this subpart.	i. Collecting and recording the monitoring and process data listed in Table 2 (operating limits) to this subpart; and ii. Reducing the monitoring and process data associated with the operating limits specified in Table 2 to this subpart; and iii. Recording the results of any control device inspections; and iv. Reporting, in accordance with §63.9814(e), any deviation from the applicable operating limits specified in Table 2 to this subpart.
2. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.	As specified in items 3 through 7 of this table.	Satisfying the applicable requirements specified in items 3 through 7 of this table.
3. Each affected process unit that is equipped with a thermal or catalytic oxidizer.	a. The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	i. Collecting the applicable data measured by the control device temperature monitoring system, as specified in items 5, 6, 8, and 9 of Table 8 to this subpart; and ii. Reducing the applicable data measured by the control device temperature monitoring system, as specified in items 5, 6, 8, and 9 of Table 8 to this subpart; and iii. Maintaining the average control device operating temperature for the applicable averaging period specified in items 5, 6, 8, and 9 of Table 2 to this subpart at or above the minimum allowable operating temperature established during the most recent performance test.
4. Each affected process unit that is equipped with a control device other than a thermal or catalytic oxidizer.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC performance reduction must equal or exceed 95 percent.	Operating and maintaining a THC CEMS at the outlet of the control device or in the stack of the affected source, according to the requirements of Procedure 1 of 40 CFR part 60, appendix F.
5. Each affected process unit that uses process changes to meet the applicable emission limit.	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen.	Operating and maintaining a THC CEMS at the outlet of the control device or in the stack of the affected source, according to the requirements of Procedure 1 of 40 CFR part 60, appendix F.
6. Each affected continuous process unit	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	Recording the organic HAP processing rate (pounds per hour) and the operating temperature of the affected source, as specified in items 3.b. and 3.c. of Table 4 to this subpart.

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For . . .	For the following emission limit . . .	You must demonstrate continuous compliance by . . .
7. Each affected batch process unit	The average THC concentration must not exceed 20 ppmvd, corrected to 18 percent oxygen; OR the average THC percentage reduction must equal or exceed 95 percent.	Recording the organic HAP processing rate (pounds per batch); and process cycle time for each batch cycle; and hourly average operating temperature of the affected source, as specified in items 8.b. through 8.d. of Table 4 to this subpart.
8. Each kiln that is used to process clay refractory products.	As specified in items 9 through 11 of this table.	Satisfying the applicable requirements specified in items 9 through 11 of this table.
9. Each affected kiln that is equipped with a DLA.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed, OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed, or the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Maintaining the pressure drop across the DLA at or above the minimum levels established during the most recent performance test; and</p> <p>ii. Verifying that the limestone hopper contains an adequate amount of free-flowing limestone by performing a daily visual check of the limestone in the feed hopper; and</p> <p>iii. Recording the limestone feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test; and</p> <p>iv. Using the same grade of limestone as was used during the most recent performance test and maintaining records of the source and grade of limestone.</p>
10. Each affected kiln that is equipped with a DIFF or DLS/FF.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Verifying at least once each 8-hour shift that lime is free-flowing by means of a visual check, checking the output of a load cell, carrier gas/lime flow indicator, or carrier gas pressure drop measurement system; and</p> <p>ii. Recording feeder setting daily to verify that the feeder setting is at or above the level established during the most recent performance test; and</p> <p>iii. Initiating corrective action within 1 hour of a bag leak detection system alarm AND completing corrective actions in accordance with the OM&M plan, AND operating and maintaining the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period.</p>
11. Each affected kiln that is equipped with a wet scrubber.	<p>a. The average HF emissions must not exceed 0.019 kg/Mg (0.038 lb/ton) of uncalcined clay processed; OR the average uncontrolled HF emissions must be reduced by at least 90 percent; and</p> <p>b. The average HCl emissions must not exceed 0.091 kg/Mg (0.18 lb/ton) of uncalcined clay processed; OR the average uncontrolled HCl emissions must be reduced by at least 30 percent.</p>	<p>i. Maintaining the pressure drop across the scrubber, liquid pH, and liquid flow rate at or above the minimum levels established during the most recent performance test; and</p> <p>ii. If chemicals are added to the scrubber liquid, maintaining the average chemical feed rate at or above the minimum chemical feed rate established during the most recent performance test.</p>

TABLE 8 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH OPERATING LIMITS

As stated in §63.9810, you must show continuous compliance with the operating limits for affected sources according to the following table:

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>1. Each affected source listed in Table 2 to this subpart.</p>	<p>a. Each applicable operating limit listed in Table 2 to this subpart.</p>	<p>i. Maintaining all applicable process and control device operating parameters within the limits established during the most recent performance test; and</p> <p>ii. Conducting annually an inspection of all duct work, vents, and capture devices to verify that no leaks exist and that the capture device is operating such that all emissions are properly vented to the control device in accordance with the OM&M plan.</p>
<p>2. Each affected continuous kiln that is equipped with a control device.</p>	<p>a. The operating limits specified in items 2.a. through 2.c. of Table 2 to this subpart.</p>	<p>i. Operating the control device on the affected kiln during all times except during periods of approved scheduled maintenance, as specified in §63.9792(e); and</p> <p>ii. Minimizing HAP emissions from the affected kiln during all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service; and</p> <p>iii. Minimizing the duration of all periods of scheduled maintenance of the kiln control device when the kiln is operating and the control device is out of service.</p>
<p>3. Each new or existing curing oven, shape dryer, and kiln that is used to process refractory products that use organic HAP; each new or existing coking oven and defumer that is used to produce pitch-impregnated refractory products; each new shape preheater that is used to produce pitch-impregnated refractory products; AND each new or existing process unit that is exhausted to a thermal or catalytic oxidizer that also controls emissions from an affected shape preheater or pitch working tank.</p>	<p>As specified in items 4 through 9 of this table.</p>	<p>Satisfying the applicable requirements specified in items 4 through 9 of this table.</p>
<p>4. Each affected continuous process unit</p>	<p>Maintain process operating parameters within the limits established during the most recent performance test.</p>	<p>i. Recording the organic HAP processing rate (pounds per hour); and</p> <p>ii. Recording the operating temperature of the affected source at least hourly; and</p> <p>iii. Maintaining the 3-hour block average organic HAP processing rate at or below the maximum organic HAP processing rate established during the most recent performance test.</p>
<p>5. Continuous process units that are equipped with a thermal oxidizer.</p>	<p>Maintain the 3-hour block average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established during the most recent performance test.</p>	<p>i. Measuring and recording the thermal oxidizer combustion chamber temperature at least every 15 minutes; and</p> <p>ii. Calculating the hourly average thermal oxidizer combustion chamber temperature; and</p> <p>iii. Maintaining the 3-hour block average thermal oxidizer combustion chamber temperature at or above the minimum allowable operating temperature established during the most recent performance test; and</p> <p>iv. Reporting, in accordance with §63.9814(e), any 3-hour block average operating temperature measurements below the minimum allowable thermal oxidizer combustion chamber operating temperature established during the most recent performance test.</p>

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>6. Continuous process units that are equipped with a catalytic oxidizer.</p>	<p>a. Maintain the 3-hour block average temperature at the inlet of the catalyst bed at or above the minimum allowable catalyst bed inlet temperature established during the most recent performance test.</p>	<p>i. Measuring and recording the temperature at the inlet of the catalyst bed at least every 15 minutes; and ii. Calculating the hourly average temperature at the inlet of the catalyst bed; and iii. Maintaining the 3-hour block average temperature at the inlet of the catalyst bed at or above the minimum allowable catalyst bed inlet temperature established during the most recent performance test; and iv. Reporting, in accordance with §63.9814(e), any 3-hour block average catalyst bed inlet temperature measurements below the minimum allowable catalyst bed inlet temperature established during the most recent performance; and v. Checking the activity level of the catalyst at least every 12 months and taking any necessary corrective action, such as replacing the catalyst, to ensure that the catalyst is performing as designed.</p>
<p>7. Each affected batch process unit</p>	<p>Maintain process operating parameters within the limits established during the most recent performance test.</p>	<p>i. Recording the organic HAP processing rate (pounds per batch); and ii. Recording the hourly average operating temperature of the affected source; and iii. Recording the process cycle time for each batch cycle; and iv. Maintaining the organic HAP processing rate at or below the maximum organic HAP processing rate established during the most recent performance test.</p>
<p>8. Batch process units that are equipped with a thermal oxidizer.</p>	<p>Maintain the hourly average temperature in the thermal oxidizer combustion chamber at or above the hourly average temperature established for the corresponding 1-hour period of the cycle during the most recent performance test.</p>	<p>i. Measuring and recording the thermal oxidizer combustion chamber temperature at least every 15 minutes; and ii. Calculating the hourly average thermal oxidizer combustion chamber temperature; and iii. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintaining the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding period during the most recent performance test, as determined according to item 11 of Table 4 to this subpart; and iv. For each subsequent hour of the batch cycle, maintaining the hourly average operating temperature in the thermal oxidizer combustion chamber at or above the minimum allowable operating temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and v. Reporting, in accordance with §63.9814(e), any temperature measurements below the minimum allowable thermal oxidizer combustion chamber temperature measured during the most recent performance test.</p>

For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>9. Batch process units that are equipped with a catalytic oxidizer.</p>	<p>Maintain the hourly average temperature at the inlet of the catalyst bed at or above the corresponding hourly average temperature established for the corresponding 1-hour period of the cycle during the most recent performance test.</p>	<p>i. Measuring and recording temperatures at the inlet of the catalyst bed at least every 15 minutes; and ii. Calculating the hourly average temperature at the inlet of the catalyst bed; and iii. From the start of each batch cycle until 3 hours have passed since the process unit reached maximum temperature, maintaining the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable bed inlet temperature established for the corresponding period during the most recent performance test, as determined according to item 12 of Table 4 to this subpart; and iv. For each subsequent hour of the batch cycle, maintaining the hourly average operating temperature at the inlet of the catalyst bed at or above the minimum allowable bed inlet temperature established for the corresponding hour during the most recent performance test, as specified in item 13 of Table 4 to this subpart; and v. Reporting, in accordance with §63.9814(e), any catalyst bed inlet temperature measurements below the minimum allowable bed inlet temperature measured during the most recent performance test; and vi. Checking the activity level of the catalyst at least every 12 months and taking any necessary corrective action, such as replacing the catalyst, to ensure that the catalyst is performing as designed.</p>
<p>10. Each new kiln that is used to process clay refractory products.</p>	<p>As specified in items 11 through 13 of this table.</p>	<p>Satisfying the applicable requirements specified in items 11 through 13 of this table.</p>
<p>11. Each new kiln that is equipped a DLA</p>	<p>a. Maintain the average pressure drop across the DLA for each 3-hour block period at or above the minimum pressure drop established during the most recent performance test.</p> <p>b. Maintain free-flowing limestone in the feed hopper, silo, and DLA.</p> <p>c. Maintain the limestone feeder setting at or above the level established during the most recent performance test.</p> <p>d. Use the same grade of limestone from the same source as was used during the most recent performance test.</p>	<p>i. Collecting the DLA pressure drop data, as specified in item 18.a. of Table 4 to this subpart; and ii. Reducing the DLA pressure drop data to 1-hour and 3-hour block averages; and iii. Maintaining the 3-hour block average pressure drop across the DLA at or above the minimum pressure drop established during the most recent performance test.</p> <p>Verifying that the limestone hopper has an adequate amount of free-flowing limestone by performing a daily visual check of the limestone hopper.</p> <p>Recording the limestone feeder setting at least daily to verify that the feeder setting is being maintained at or above the level established during the most recent performance test.</p> <p>Using the same grade of limestone as was used during the most recent performance test and maintaining records of the source and grade of limestone.</p>

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For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
<p>12. Each new kiln that is equipped with a DIFF or DLS/FF.</p>	<p>a. Initiate corrective action within 1 hour of a bag leak detection system alarm and complete corrective actions in accordance with the OM&M plan; AND operate and maintain the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period.</p> <p>b. Maintain free-flowing lime in the feed hopper or silo at all times for continuous injection systems; AND maintain feeder setting at or above the level established during the most recent performance test for continuous injection systems.</p>	<p>i. Initiating corrective action within 1 hour of a bag leak detection system alarm and completing corrective actions in accordance with the OM&M plan; and</p> <p>ii. Operating and maintaining the fabric filter such that the alarm does not engage for more than 5 percent of the total operating time in a 6-month block reporting period; in calculating this operating time fraction, if inspection of the fabric filter demonstrates that no corrective action is required, no alarm time is counted; if corrective action is required, each alarm shall be counted as a minimum of 1 hour; if you take longer than 1 hour to initiate corrective action, the alarm time shall be counted as the actual amount of time taken by you to initiate corrective action.</p> <p>i. Verifying at least once each 8-hour shift that lime is free-flowing via a load cell, carrier gas/lime flow indicator, carrier gas pressure drop measurement system, or other system; recording all monitor or sensor output, and if lime is found not to be free flowing, promptly initiating and completing corrective actions; and</p> <p>ii. Recording the feeder setting once each day of operation to verify that the feeder setting is being maintained at or above the level established during the most recent performance test.</p>
<p>13. Each new kiln that is used to process clay refractory products and is equipped with a wet scrubber.</p>	<p>a. Maintain the average pressure drop across the scrubber for each 3-hour block period at or above the minimum pressure drop established during the most recent performance test.</p> <p>b. Maintain the average scrubber liquid pH for each 3-hour block period at or above the minimum scrubber liquid pH established during the most recent performance test.</p> <p>c. Maintain the average scrubber liquid flow rate for each 3-hour block period at or above the minimum scrubber liquid flow rate established during the most recent performance test.</p> <p>d. If chemicals are added to the scrubber liquid, maintain the average scrubber chemical feed rate for each 3-hour block period at or above the minimum scrubber chemical feed rate established during the most recent performance test.</p>	<p>i. Collecting the scrubber pressure drop data, as specified in item 20.a. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber pressure drop data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber pressure drop at or above the minimum pressure drop established during the most recent performance test.</p> <p>i. Collecting the scrubber liquid pH data, as specified in item 20.b. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber liquid pH data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber liquid pH at or above the minimum scrubber liquid pH established during the most recent performance test.</p> <p>i. Collecting the scrubber liquid flow rate data, as specified in item 20.c. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber liquid flow rate data to 1-hour and 3-hour block averages; and</p> <p>iii. Maintaining the 3-hour block average scrubber liquid flow rate at or above the minimum scrubber liquid flow rate established during the most recent performance test.</p> <p>i. Collecting the scrubber chemical feed rate data, as specified in item 20.d. of Table 4 to this subpart; and</p> <p>ii. Reducing the scrubber chemical feed rate data to 1-hour and 3-hour block averages; and</p>

For . . .	For the following operating limit . . .	You must demonstrate continuous compliance by . . .
		iii. Maintaining the 3-hour block average scrubber chemical feed rate at or above the minimum scrubber chemical feed rate established during the most recent performance test.

TABLE 9 TO SUBPART SSSSS OF PART 63—CONTINUOUS COMPLIANCE WITH WORK PRACTICE STANDARDS

As stated in §63.9810, you must show continuous compliance with the work practice standards for affected sources according to the following table:

For . . .	For the following work practice standard . . .	You must demonstrate continuous compliance by . . .
1. Each affected source listed in Table 3 to this subpart.	Each applicable work practice requirement listed in Table 3 to this subpart.	i. Performing each applicable work practice standard listed in Table 3 to this subpart; and ii. Maintaining records that document the method and frequency for complying with each applicable work practice standard listed in Table 3 to this subpart, as required by §§63.10(b) and 63.9816(c)(2).
2. Each basket or container that is used for holding fired refractory shapes in an existing shape preheater and autoclave during the pitch impregnation process.	Control POM emissions from any affected shape preheater.	i. Controlling emissions from the volatilization of residual pitch by implementing one of the work practice standards listed in item 1 of Table 3 to this subpart; and ii. Recording the date and cleaning method each time you clean an affected basket or container.
3. Each new or existing pitch working tank	Control POM emissions	Capturing and venting emissions from the affected pitch working tank to the control device that is used to control emissions from an affected defumer or coking oven, or to a thermal or catalytic oxidizer that is comparable to the control device used on an affected defumer or coking oven.
4. Each new or existing chromium refractory products kiln.	Minimize fuel-basec HAP emissions	i. Using natural gas, or equivalent, as the kiln fuel at all times except during periods of natural gas curtailment or supply interruption; and ii. If you intend to use an alternative fuel, submitting a notification of alternative fuel use within 48 hours of the declaration of a period of natural gas curtailment or supply interruption, as defined in §63.9824; and iii. Submitting a report of alternative fuel use within 10 working days after terminating the use of the alternative fuel, as specified in §63.9814(g).
5. Each existing clay refractory products kiln.	Minimize fuel-basec HAP emissions	i. Using natural gas, or equivalent, as the kiln fuel at all times except during periods of natural gas curtailment or supply interruption; and ii. If you intend to use an alternative fuel, submitting a notification of alternative fuel use within 48 hours of the declaration of a period of natural gas curtailment or supply interruption, as defined in §63.9824; and iii. Submitting a report of alternative fuel use within 10 working days after terminating the use of the alternative fuel, as specified in §63.9814(g).

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TABLE 10 TO SUBPART SSSSS OF PART 63—REQUIREMENTS FOR REPORTS

As stated in §63.9814, you must comply with the requirements for reports in the following table:

You must submit a(n) . . .	The report must contain . . .	You must submit the report . . .
1. Compliance report	The information in §63.9814(c) through (f).	Semiannually according to the requirements in §63.9814(a) through (f).
2. Immediate startup, shutdown, and malfunction report if you had a startup, shutdown, or malfunction during the reporting period that is not consistent with your SSMP.	a. Actions taken for the event	By fax or telephone within 2 working days after starting actions inconsistent with the plan.
	b. The information in §63.10(d)(5)(ii)	By letter within 7 working days after the end of the event unless you have made alternative arrangements with the permitting authority.
3. Report of alternative fuel use	The information in §63.9814(g) and items 4 and 5 of Table 9 to this subpart.	If you are subject to the work practice standard specified in item 3 or 4 of Table 3 to this subpart, and you use an alternative fuel in the affected kiln, by letter within 10 working days after terminating the use of the alternative fuel.

TABLE 11 TO SUBPART SSSSS OF PART 63—APPLICABILITY OF GENERAL PROVISIONS TO SUBPART SSSSS

As stated in §63.9820, you must comply with the applicable General Provisions requirements according to the following table:

Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.1	Applicability	Yes.
§ 63.2	Definitions	Yes.
§ 63.3	Units and Abbreviations	Yes.
§ 63.4	Prohibited Activities	Compliance date; circumvention, severability.	Yes.
§ 63.5	Construction/Reconstruction	Applicability; applications; approvals	Yes.
§ 63.6(a)	Applicability	General Provisions (GP) apply unless compliance extension; GP apply to area sources that become major.	Yes.
§ 63.6(b)(1)–(4) ..	Compliance Dates for New and Reconstructed Sources.	Standards apply at effective date; 3 years after effective date; upon startup; 10 years after construction or reconstruction commences for section 112(f).	Yes.
§ 63.6(b)(5)	Notification	Yes.
§ 63.6(b)(6)	[Reserved]		
§ 63.6(b)(7)	Compliance Dates for New and Reconstructed Area Sources That Become Major.	Area sources that become major must comply with major source standards immediately upon becoming major, regardless of whether required to comply when they were area sources.	Yes.
§ 63.6(c)(1)–(2) ..	Compliance Dates for Existing Sources ...	Comply according to date in subpart, which must be no later than 3 years after effective date; for section 112(f) standards, comply within 90 days of effective date unless compliance extension.	Yes.
§ 63.6(c)(3)–(4) ..	[Reserved]		
§ 63.6(c)(5)	Compliance Dates for Existing Area Sources That Become Major.	Area sources that become major must comply with major source standards by date indicated in subpart or by equivalent time period (for example, 3 years).	Yes.
§ 63.6(d)	[Reserved]		
§ 63.6(e)(1)–(2) ..	Operation & Maintenance	Operate to minimize emissions at all times; correct malfunctions as soon as practicable; requirements independently enforceable; information Administrator will use to determine if operation and maintenance requirements were met.	Yes.

Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.6(e)(3)	Startup, Shutdown, and Malfunction Plan (SSMP)	Yes.
§ 63.6(f)(1)	Compliance Except During SSM	You must comply with emission standards at all times except during SSM.	Yes.
§ 63.6(f)(2)-(3) ..	Methods for Determining Compliance	Compliance based on performance test, operation and maintenance plans, records, inspection.	Yes.
§ 63.6(g)(1)-(3) ..	Alternative Standard	Procedures for getting an alternative standard.	Yes.
§ 63.6(h)(1)-(9) ..	Opacity/Visible Emission (VE) Standards	Not applicable.
§ 63.6(i)(1)-(14) ..	Compliance Extension	Procedures and criteria for Administrator to grant compliance extension.	Yes.
§ 63.6(j)	Presidential Compliance Exemption	President may exempt source category ...	Yes.
§ 63.7(a)(1)-(2) ..	Performance Test Dates	Dates for conducting initial performance testing and other compliance demonstrations; must conduct 180 days after first subject to rule.	Yes.
§ 63.7(a)(3)	Section 114 Authority	Administrator may require a performance test under CAA section 114 at any time.	Yes.
§ 63.7(b)(1)	Notification of Performance Test	Must notify Administrator 60 days before the test.	Yes.
§ 63.7(b)(2)	Notification of Rescheduling	Must notify Administrator 5 days before scheduled date and provide rescheduled date.	Yes.
§ 63.7(c)	Quality Assurance/Test Plan	Requirements; test plan approval procedures; performance audit requirements; internal and external QA procedures for testing.	Yes.
§ 63.7(d)	Testing Facilities	Yes.
§ 63.7(e)(1)	Conditions for Conducting Performance Tests.	Performance tests must be conducted under representative conditions; cannot conduct performance tests during SSM; not a violation to exceed standard during SSM.	No, § 63.9800 specifies requirements; Yes; Yes.
§ 63.7(e)(2)	Conditions for Conducting Performance Tests.	Must conduct according to subpart and EPA test methods unless Administrator approves alternative.	Yes.
§ 63.7(e)(3)	Test Run Duration	Must have three test runs of at least 1 hour each; compliance is based on arithmetic mean of three runs; conditions when data from an additional test run can be used.	Yes; Yes, except where specified in § 63.9800 for batch process sources; Yes.
§ 63.7(f)	Alternative Test Method	Yes.
§ 63.7(g)	Performance Test Data Analysis	Yes.
§ 63.7(h)	Waiver of Test	Yes.
§ 63.8(a)(1)	Applicability of Monitoring Requirements	Yes.
§ 63.8(a)(2)	Performance Specifications	Performance Specifications in appendix B of 40 CFR part 60 apply.	Yes.
§ 63.8(a)(3)	[Reserved]
§ 63.8(a)(4)	Monitoring with Flares	Not applicable.
§ 63.8(b)(1)	Monitoring	Must conduct monitoring according to standard unless Administrator approves alternative.	Yes.
§ 63.8(b)(2)-(3) ..	Multiple Effluents and Multiple Monitoring Systems.	Specific requirements for installing and reporting on monitoring systems.	Yes.
§ 63.8(c)(1)	Monitoring System Operation and Maintenance.	Maintenance consistent with good air pollution control practices.	Yes.
§ 63.8(c)(1)(i)	Routine and Predictable SSM	Reporting requirements for SSM when action is described in SSMP.	Yes.
§ 63.8(c)(1)(ii)	SSM not in SSMP	Reporting requirements for SSM when action is not described in SSMP.	Yes.
§ 63.8(c)(1)(iii)	Compliance with Operation and Maintenance Requirements.	How Administrator determines if source is complying with operation and maintenance requirements.	Yes.
§ 63.8(c)(2)-(3) ..	Monitoring System Installation	Must install to get representative emission and parameter measurements.	Yes.
§ 63.8(c)(4)	CMS Requirements	No, § 63.9808 specifies requirements.
§ 63.8(c)(5)	COMS Minimum Procedures	Not applicable.
§ 63.8(c)(6)	CMS Requirements	Applies only to sources required to install and operate a THC CEMS.

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Citation	Subject	Brief description	Applies to subpart SSSSS
§ 63.8(c)(7)(i)(A)	CMS Requirements	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(c)(7)(i)(B)	CMS Requirements	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(c)(7)(i)(C)	CMS Requirements	Not applicable.
§ 63.8(c)(7)(ii)	CMS Requirements	Corrective action required when CMS is out of control.	Yes.
§ 63.8(c)(8)	CMS Requirements	Yes.
§ 63.8(d)	CMS Quality Control	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(e)	CMS Performance Evaluation	Applies only to sources required to install and operate a THC CEMS.
§ 63.8(f)(1)–(5) ..	Alternative Monitoring Method	Yes.
§ 63.8(f)(6)	Alternative to Relative Accuracy Test	Yes.
§ 63.8(g)	Data Reduction	Applies only to sources required to install and operate a THC CEMS.
§ 63.9(a)	Notification Requirements	Yes.
§ 63.9(b)(1)–(5) ..	Initial Notifications	Yes.
§ 63.9(c)	Request for Compliance Extension	Yes.
§ 63.9(d)	Notification of Special Compliance Requirements for New Source.	Yes.
§ 63.9(e)	Notification of Performance Test	Notify Administrator 60 days prior	Yes.
§ 63.9(f)	Notification of VE/Opacity Test	Not applicable.
§ 63.9(g)	Additional Notifications When Using CMS	Applies only to sources required to install and operate a THC CEMS.
§ 63.9(h)	Notification of Compliance Status	Yes.
§ 63.9(i)	Adjustment of Submittal Deadlines	Yes.
§ 63.9(j)	Change in Previous Information	Yes.
§ 63.10(a)	Recordkeeping/Reporting	Yes.
§ 63.10(b)(1)	Recordkeeping/Reporting	Yes.
§ 63.10(b)(2)(i)–(v).	Records Related to Startup, Shutdown, and Malfunction.	Yes.
§ 63.10(b)(2)(vi) and (x–xi).	CMS Records	Yes.
§ 63.10(b)(2)(vii)–(ix).	Records	Measurements to demonstrate compliance with emission limitations; performance test, performance evaluation, and visible emission observation results; measurements to determine conditions of performance tests and performance evaluations.	Yes.
§ 63.10(b)(2)(xii)	Records	Records when under waiver	Yes.
§ 63.10(b)(2)(xiii)	Records	Records when using alternative to relative accuracy test.	Not applicable.
§ 63.10(b)(2)(xiv)	Records	All documentation supporting Initial Notification and Notification of Compliance Status.	Yes.
§ 63.10(b)(3)	Records	Applicability Determinations	Yes.
§ 63.10(c)(1)–(6), (9)–(15).	Records	Additional Records for CMS	Not applicable.
§ 63.10(c)(7)–(8)	Records	Records of excess emissions and parameter monitoring exceedances for CMS.	No, § 63.9816 specifies requirements.
§ 63.10(d)(1)	General Reporting Requirements	Requirements for reporting	Yes.
§ 63.10(d)(2)	Report of Performance Test Results	When to submit to Federal or State authority.	Yes.
§ 63.10(d)(3)	Reporting Opacity or VE Observations	Not applicable.
§ 63.10(d)(4)	Progress Reports	Must submit progress reports on schedule if under compliance extension.	Yes.
§ 63.10(d)(5)	Startup, Shutdown, and Malfunction Reports.	Contents and submission	Yes.

Citation	Subject	Brief description	Applies to subpart SSSS
§ 63.10(e)(1)-(2)	Additional CMS Reports	Applies only to sources required to install and operate a THC CEMS. No. § 63.9814 species requirements. Not applicable. Yes. Not applicable. Yes. Yes. Yes. Yes.
§ 63.10(e)(3)	Reports	
§ 63.10(e)(4)	Reporting COMS data	
§ 63.10(f)	Waiver for Recordkeeping/Reporting	
§ 63.11	Flares	
§ 63.12	Delegation	
§ 63.13	Addresses	
§ 63.14	Incorporation by Reference	
§ 63.15	Availability of Information	

Subpart TTTT—National Emissions Standards for Hazardous Air Pollutants for Primary Magnesium Refining

SOURCE: 68 FR 58620, Oct. 10, 2003, unless otherwise noted.

WHAT THIS SUBPART COVERS

§ 63.9880 What is the purpose of this subpart?

This subpart establishes national emission standards for hazardous air pollutants (NESHAP) for primary magnesium refineries. This subpart also establishes requirements to demonstrate initial and continuous compliance with all applicable emission limitations, work practice standards, and operation and maintenance requirements.

§ 63.9881 Am I subject to this subpart?

You are subject to this subpart if you own or operate a primary magnesium refinery that is (or is part of) a major source of hazardous air pollutant (HAP) emissions. Your primary magnesium refinery is a major source of HAP if it emits or has the potential to emit any single HAP at a rate of 10 tons or more per year or any combination of HAP at a rate of 25 tons or more per year.

§ 63.9882 What parts of my plant does this subpart cover?

(a) The affected sources are each new and existing primary magnesium refining facility.

(b) This subpart covers emissions from each spray dryer stack, magnesium chloride storage bins scrubber stack, melt/reactor system stack, and

launder off-gas system stack at your primary magnesium refining facility. This subpart also covers fugitive dust emissions.

(c) Each primary magnesium refining facility is existing if you commenced construction or reconstruction of the affected source before January 22, 2003.

(d) Each primary magnesium refining facility is new if you commence construction or reconstruction of the affected source on or after January 22, 2003. An affected source is reconstructed if it meets the definition of reconstruction in § 63.2.

§ 63.9883 When do I have to comply with this subpart?

(a) If you have an existing source, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you no later than October 11, 2004.

(b) If you have a new affected source and its initial startup date is on or before October 11, 2003, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you by October 10, 2003.

(c) If you have a new affected source and its initial startup date is after October 10, 2003, you must comply with each emission limitation, work practice standard, and operation and maintenance requirement in this subpart that applies to you upon initial startup.

(d) If your primary magnesium refinery is an area source that becomes a major source of HAP, the compliance